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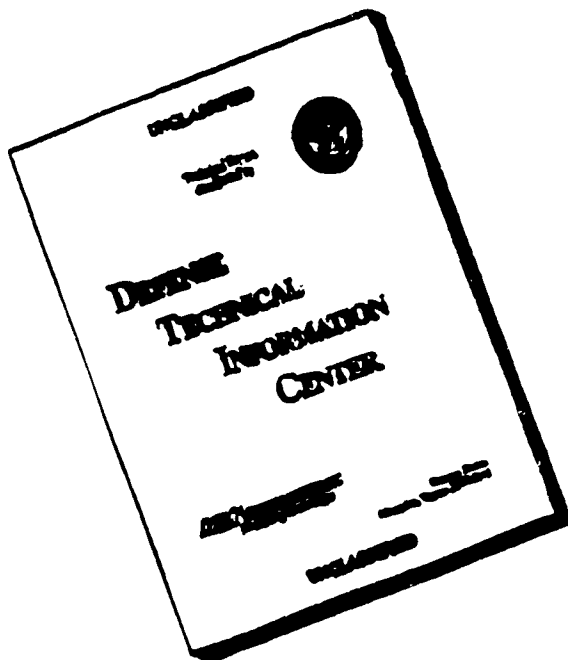
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NAVORD REPORT

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THEORETICAL INVESTIGATION OF TURBULENT BOUNDARY LAYER FLOW  
WITH HEAT TRANSFER AT SUPERSONIC AND HYPERSONIC SPEEDS

19 MAY 1955



**U. S. NAVAL ORDNANCE LABORATORY**  
**WHITE OAK, MARYLAND**

NAVORD Report 3854

Acroballistic Research Report 258

**A THEORETICAL INVESTIGATION OF TURBULENT  
BOUNDARY LAYER FLOW WITH HEAT TRANSFER  
AT SUPERSONIC AND HYPERSONIC SPEEDS**

Prepared by:

Jerome Persh

**ABSTRACT:** A theoretical investigation of compressible turbulent boundary layer flow with and without steady state heat transfer has been conducted. This investigation is based on a simple physical model of the flow suggested first by Prandtl and used later by Donaldson. The physical model consists of a laminar sublayer region with a linear velocity profile and an outer turbulent portion with a power law velocity profile. Comparisons between theory and experiment demonstrate that the analysis yields good results for compressible turbulent boundary layer flow with and without steady state heat transfer.

U. S. NAVAL ORDNANCE LABORATORY  
WHITE OAK, MARYLAND

19 May 1955

This report contains the results of a theoretical investigation of compressible turbulent boundary layer flow with and without steady state heat transfer. The significance of this work is apparent when it is considered that although a great deal of experimental and theoretical information exists for supersonic turbulent boundary layers in the absence of heat transfer, there are relatively few detailed investigations in the supersonic and hypersonic speed ranges that include the effects of heat transfer.

The work was jointly sponsored by the U. S. Naval Bureau of Ordnance and the U. S. Air Force, and was performed under Tasks NOL-M9a-133-1-55 and NOL-M9a-133-5-55. The author is deeply indebted to Dr. R. E. Wilson and Dr. R. K. Lobb for their guidance and continued interest during the course of the investigation, and to Mrs. Leah Brown of the Applied Mathematics Division, who carried out the computation of the data contained in Table I.

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## SYMBOLS

- $c_f$  - Local skin friction coefficient based on free-stream conditions,  $2 \tau_w / \rho_\infty u_\infty^2$
- $C_F$  - Mean skin friction coefficient based on free-stream conditions,  $\frac{2D}{\rho_\infty u_\infty^2 x}$
- $c_{fi}$  - Incompressible local skin friction coefficient for zero heat transfer based on free-stream conditions
- $C_{Fi}$  - Incompressible mean skin friction coefficient for zero heat transfer based on free-stream conditions
- $D$  - Drag force
- $H$  - Boundary layer shape parameter,  $g^*/\theta$
- $k$  - Constant in mixing length law
- $l$  - Mixing length
- $M$  - Mach number
- $n$  - Exponent in power law velocity profile representation
- $r$  - Ratio of total shear stress to viscous shear stress
- $r.f.$  - Recovery factor
- $Re$  - Reynolds number
- $T$  - Local static temperature
- $u$  - Mean velocity component in x-direction
- $u^+$  - Velocity parameter,  $u/u_\tau$  (based on wall conditions)
- $u_\tau$  - Friction velocity  $\sqrt{\tau_w/\rho_w}$
- $x$  - Axial distance along surface
- $y$  - Distance perpendicular to surface
- $y^+$  - Wall distance parameter,  $y u_\tau / \nu$  (based on wall conditions)



SYMBOLS (continued)

- $\delta$  - Total boundary layer thickness
- $\delta^*$  - Boundary layer displacement thickness,  $\int_0^\delta \left[ 1 - \frac{\rho u}{\rho_\infty u_\infty} \right] dy$
- $\theta$  - Boundary layer momentum thickness,  $\int_0^\delta \frac{\rho u}{\rho_\infty u_\infty} \left[ 1 - \frac{u}{u_\infty} \right] dy$
- $\mu$  - Viscosity
- $\nu$  - Kinematic viscosity
- $\rho$  - Density
- $\tau_{Lam.}$  - Laminar shear stress
- $\tau_{Turb.}$  - Turbulent shear stress
- $\omega$  - Exponent in viscosity-temperature relationship

Subscripts:

- e - Equilibrium wall temperature
- L - Values at the edge of laminar sublayer
- T - Turbulent region
- w - Values based on wall conditions
- x - Values based on distance from leading edge of plate
- $\delta$  - Values based on boundary layer thickness
- $\theta$  - Values based on boundary layer momentum thickness
- $\infty$  - Values based on free-stream conditions outside boundary layer

A THEORETICAL INVESTIGATION OF TURBULENT  
BOUNDARY LAYER FLOW WITH HEAT TRANSFER  
AT SUPERSONIC AND HYPERSONIC SPEEDS

INTRODUCTION

1. Despite a lack of experimental data, numerous formulae have been developed for the variation of turbulent skin friction on a flat plate, with and without steady state heat transfer. The reports of Rubesin, Maydew, and Varga (reference a), and Chapman and Kester (reference b) include good resumes of several theoretical treatments of this problem. All of the analyses reviewed in these references make use of empirical constants which are drawn from incompressible experimental data. Recent experimental results (reference c) have demonstrated that the empirical incompressible constants utilized are affected by heat transfer. Specifically, it has been found that the assumption that the edge of the laminar sublayer occurs at fixed values of the parameters  $u_L^+$  (or  $y_L^+$ ) is not strictly valid. Experimental results indicate that the value of  $u_L^+$  does not only vary with heat transfer, but to some extent with Reynolds number and Mach number. It was felt, therefore, that a theoretical approach which is based on a realistic physical model of the flow, and which allows a prediction of the quantities at the edge of the laminar sublayer, is expedient at the present time.
2. Such an approach was originally devised by Prandtl (reference d) and recently extended to compressible flows by Donaldson (reference e). The physical model of a turbulent boundary layer proposed by these investigators may be briefly described as follows: It is assumed that the turbulent boundary layer velocity profile can be divided into two regions; the wall adjacent region called the laminar sublayer, where the velocity varies linearly with distance from the surface, and the outer turbulent portion, which is represented by a power profile. The intersection of these two profiles is defined as the edge of the laminar sublayer.
3. It is the purpose of this investigation to extend and revise the analysis of Donaldson in order to obtain consistency with the most recent and reliable experimental results for low speed turbulent boundary layers. The applicability of this analysis for compressible turbulent boundary layers with and without steady state heat transfer is demonstrated by comparisons with supersonic and hypersonic experimental results.

# ANALYSIS

## Incompressible Turbulent Boundary Layers

4. It has been established by numerous investigators that the velocity profile in the outer turbulent portion of the boundary layer may be adequately represented by a power profile of the form

$$\frac{u}{u_{\infty}} = \left[ \frac{y}{\delta} \right]^{\frac{1}{n}} \quad \delta_L \leq y \leq \delta \quad (1)$$

while experimental evidence indicates that, in the laminar sub-layer region, the velocity profile is essentially a straight line

$$\frac{u}{u_L} = \frac{y}{\delta_L} \times \text{constant} \quad 0 \leq y \leq \delta_L \quad (2)$$

The boundary layer is thus divided into a turbulent portion described by Eq. (1) and a laminar region having a linear velocity profile (Eq. 2). This is shown in Figure 1 with the real conditions in the transition region indicated by a dashed line.

5. Several general relations for the local skin friction coefficient can be deduced using the preceding postulates regarding the boundary layer velocity profile together with various assumptions regarding the shear stress at the edge of the laminar sublayer. These relations necessarily embody unknown functions which must be evaluated empirically.

6. Donaldson (reference e) introduced an empirical constant relating the total shear stress and the laminar shear stress in order to compute the skin friction. Taking

$$\frac{\tau_{Lam.} + \tau_{Turb.}}{\tau_{Lam.}} = r = \text{constant} \quad (3)$$

and evaluating  $r$  at  $y = \delta_L$  from the power profile given by Eq. (1), Donaldson (reference e) derived the following relation for the skin friction coefficient

$$c_{f1} = 2 \left[ \frac{n(r-1)}{k^2} \right] \frac{1-n}{1+n} \left[ \frac{1}{Re_{\delta}} \right]^{\frac{2}{n+1}} \quad (4)$$

and evaluated the constant  $(r-1)/k^2$  empirically using Blasius' (reference d) skin friction law. In Donaldson's analysis, the velocity profile exponent (n) is considered constant, and the Prandtl mixing length law

$$l = k y \quad (5)$$

is assumed in order to calculate the turbulent shear stress,  $\tau_{\text{Turb.}}$ \*

7. In the present report the velocity profile exponent (n) was taken as a variable and the method by which Eq. (4) was correlated with experiment is as follows: First, Eq. (4) was equated to the Karman-Schoenherr incompressible skin friction law

$$C_{fi} = \frac{0.0568}{[\log_{10} (2Re_0)] [\log_{10} (2Re_0) + 0.868]} \quad (6)$$

which is regarded as a good representation of incompressible turbulent boundary layer skin friction coefficients over a wide Reynolds number range. This procedure yielded a variation of n with  $Re_0$ . A comparison was then made between experimental data and the deduced variation of n with  $Re_0$ . This approach seemed logical because the experimental variation of n with  $Re_0$  is well

\* An examination of Figure 2 suggests that since the shear stress is nearly constant near the wall, an alternate assumption regarding the relationship between the laminar and turbulent shear stress may be made. Within the sublayer the laminar shear stress predominates while outside the sublayer the turbulent shear stress predominates, and since the transition region is neglected in the model for the velocity profile, the values of  $\tau_{\text{Turb.}}$  calculated from Eq. (1) and  $\tau_{\text{Lam.}}$  calculated from Eq. (2) may be taken as each equal to the total shear stress at  $y = \delta_1$ . Thus a logical relationship between  $\tau_{\text{Turb.}}$  and  $\tau_{\text{Lam.}}$  would appear to be

$$\tau_{\text{Turb.}} = \tau_{\text{Lam.}} \text{ at } y = \delta_1$$

if  $\tau_{\text{Turb.}}$  and  $\tau_{\text{Lam.}}$  are computed as indicated above. In addition, if the von Karman mixing length formula

$$l = k \frac{du}{\frac{d^2u}{dy^2}}$$

is used instead of the Prandtl mixing length formula, each of the shear stress assumptions will lead to another skin friction relation.

A study was therefore made to determine which of the assumptions and mixing length formula yielded a skin friction law which gave the best overall agreement between theory and experiment. It was found that Eq. (4) given by Donaldson, could best be adapted to the experimental results. The details of this analysis are contained in Appendix A.

described by a large amount of experimental velocity profile data. It was found that using this procedure and taking  $\frac{r-1}{k^2}$

as constant resulted in a variation of  $n$  with  $Re_0$  which is a good average of the available experimental data (references c, f, g, and h). This is shown in Figure 3. The value of the constant  $\frac{r-1}{k^2}$  compatible with the  $n$  variation with  $Re_0$  shown

in Figure 3 is 20.0. This is only slightly different from the value of 22.5 given by Donaldson (reference e). Since in his analysis the  $n$  variation with Reynolds number was not considered and the Blasius (reference d) skin friction law was used to obtain the constant, it is to be expected that a slightly different constant would be obtained. The incompressible portion of the present analysis therefore represents an extension of the Donaldson analysis in that the  $n$  variation with Reynolds number is considered.

### Compressible Turbulent Boundary Layers

8. Since for compressible flow, the temperature varies across the boundary layer, it is apparent that the assumption of constant shear stress through the laminar sublayer violates the stipulation that the velocity varies linearly with distance from the surface. It is assumed that this incompatibility does not introduce any serious errors in the skin friction results. The subsequent comparisons between theory and experiment tend to confirm this assumption.

9. The extension of the foregoing analysis to compressible flows is straightforward and the equations take the same form as those given in reference (e). If the value of the constant  $r$  obtained by the procedure described above is assumed to be the same for both incompressible and compressible flows with and without heat transfer, then Eq. (4) is valid for these cases if the density and viscosity contained in the Reynolds number are evaluated at the edge of the laminar sublayer. It is desirable, however, that the Reynolds number be expressed in terms of free-stream properties. This transformation is presented in reference (e) and in Appendix B where it is shown that the resulting equations necessary to determine local skin friction coefficients are as follows:

$$c_f = 2 \left[ 20 n \right]^{\frac{1-n}{1+n}} \left[ \frac{1}{Re_0 \left( \frac{\delta}{\delta^*} \right)} \right]^{\frac{2}{n+1}} \left[ \frac{T_\infty}{T_L} \right]^{\frac{n-2\omega-1}{n+1}} \quad (7)$$

$$\frac{T_L}{T_\infty} = 1 + r.f. \frac{\gamma-1}{2} M_\infty^2 \left[ 1 - \left( \frac{u_L}{u_\infty} \right)^2 \right] + \frac{T_w - T_\infty}{T_\infty} \left[ 1 - \frac{u_L}{u_\infty} \right] \quad (8)$$

$$\frac{u_L}{u_\infty} = \left[ \frac{20 n}{Re_\theta \left( \frac{\delta}{\theta} \right)} \right]^{\frac{1}{n+1}} \times \left\{ 1 + r.f. \frac{\gamma - 1}{2} M_\infty^2 \left[ 1 - \left( \frac{u_L}{u_\infty} \right)^2 \right] + \frac{T_w - T_e}{T_\infty} \left[ 1 - \frac{u_L}{u_\infty} \right] \right\}^{\frac{1.76}{n+1}} \quad (9)$$

10. Values of  $n$  for use in these equations are obtained from the curve of Figure 3. Using this single curve as a determining factor for  $n$  implies that  $n$  is uniquely related to  $Re_\theta$  regardless of Mach number or heat transfer condition. Although the results shown in Figure 3 tend to justify this postulate, probably the Mach number and heat transfer influences on  $n$  are concealed by the insensitivity inherent in this coordinate system. A comparison between a plot of  $n$  versus  $Re_\theta$  and  $n$  versus  $Re_\delta$  indicates that some influence of Mach number and heat transfer is probably incorporated in both figures, but is appreciably less in the  $Re_\theta$  plot. It is felt, therefore, that a more accurate determination of  $n$  may be obtained when  $Re_\theta$  is used as the correlating factor.

11. Since  $Re_\theta$  was chosen as the correlating factor for  $n$  and Eq. (7) requires the use of  $Re_\delta$ , a means is therefore needed for converting given values of  $Re_\theta$  to the equivalent  $Re_\delta$ . The needed  $\theta/\delta$  values have been calculated using the definition for  $\theta$  with Eq. (1) and the Orocco temperature distribution (reference e) for a series of Mach numbers up to 20, a wide range of heat transfer conditions, and  $n$  values of 5, 7, 9, and 11. These are tabulated in Table I. Also tabulated for the same range of variables are the values of  $\delta^*/\delta$  and  $H$ . It should be noted that the foregoing procedure for calculating these parameters ignores the laminar sublayer because the power profile is assumed to exist to the wall. While this procedure is not quite exact, it is felt that only small errors will result because by far the largest contributions to the integrals for  $\delta^*$  and  $\theta$  occur outside the laminar sublayer.

12. Using the present analysis, skin friction coefficients can be calculated if the Reynolds number is given in terms of either the total boundary layer thickness ( $Re_\delta$ ) or the boundary layer momentum thickness ( $Re_\theta$ ), or, as will be shown later, in terms of the distance from the leading edge. Since the dependence of  $\theta/\delta$  with Mach number and heat transfer is not considered in Donaldson's (reference e) analysis, the skin friction coefficient can be evaluated only if the value of  $Re_\delta$  is known.

13. Whether or not the postulated uniqueness of  $n$  with  $Re_\theta$  leads to serious errors may be checked by comparing the influence of  $n$  on  $c_f$  over a range of Mach numbers for a fixed value of  $Re_\theta$ . A value of  $Re_\theta$  of 8000 was selected for the check procedure,

and the  $n$  value was varied between 5.5 and 7.5 which encompasses the scatter of the experimental data at this point. It was found that the values of  $c_f$  over a range of Mach numbers up to 10 were no more than 6 percent above or below the curve drawn for the value of  $n$  theoretically associated with an  $Re_\theta$  of 8000. On the basis of this check it was concluded that the skin friction values obtained from the present analysis are not particularly sensitive to the value of  $n$  associated with the  $Re_\theta$  in question.

14. This result enables the approximate calculation of the variation of  $c_f/c_{f1}$  as a function of  $Re_x$ . If  $c_f/c_{f1}$  is not particularly sensitive to  $n$ , it may be assumed that for a given Mach number and heat transfer rate, the value of  $\theta/\delta$  along a plate is constant. This assumption is necessary to perform the integration indicated in Appendix C. Using this assumption, a relation between  $Re_\theta$  and  $Re_x$  may be deduced. The details of this derivation are given in Appendix C, where it is shown that the resulting equation is

$$Re_\theta = Re_x \frac{n+1}{n+3} \times \left\{ \left( \frac{\delta}{\theta} \right)^{n+1} \left( \frac{n+3}{n+1} \right)^{n+1} \left( \frac{1}{20n} \right)^{n-1} \left( \frac{T_\infty}{T_L} \right)^{n-2.52} \right\}^{\frac{1}{n+3}} \quad (10)$$

It is not stipulated, however, that the value of  $(n)$  for use in equation (10) is a constant. Curves showing the variation of  $c_f/c_{f1}$  as a function of Mach number for several constant values of wall temperature ratio and a constant value of  $Re_x$  of  $10^7$  (Figure 15) calculated using the equations of Appendix C are in good agreement with the empirical curves of Seif<sup>2</sup> (reference a). Results obtained using the equations of Appendix C should therefore suffice for most engineering applications.

15. The recent acquisition of detailed experimental data at hypersonic Mach numbers at both the Naval Ordnance Laboratory and the Applied Physics Laboratory (references c and f), both with and without steady state heat transfer, made it possible to examine not only the overall results of the theory but also the validity of the assumptions made and the use of constants drawn from incompressible flow results.

16. The first step is to examine the conditions at the edge of the laminar sublayer. This is necessary because the theory is focused on this point. For incompressible flows it has long been assumed that the value of  $u_L^+ = y_L^+$  at the edge of the laminar sublayer (in the logarithmic velocity profile representation) is roughly a constant that lies between 11.0 and 12.0. The present analysis is not based on this assumption but is so constructed that a computation and check of the results obtained for this point may be made.

17. The theoretical variation of  $u_L^+$  with  $Re_0$  is compared with experimental data (references i and j) for incompressible flow in Figure 4. It is apparent that the accepted presumption that  $u_L^+ = y_L^+$  is a constant is not far from true; however, the theory and experiment indicate that Reynolds number does influence the value of  $u_L^+ = y_L^+$  slightly.

18. Figure 5 shows a comparison between the theoretical and experimental values (references c, f, and k) of  $u_L^+ = y_L^+$  for compressible flow. For this comparison all values of  $u_L^+ = y_L^+$  are based on wall properties. The theoretical curves associated with each set of experimental data were calculated such that they encompassed the experimental Mach number and Reynolds number range. Although the present analysis does not accurately predict the numerical values of  $u_L^+ = y_L^+$  it does predict the proper trend of the data for both the heating and cooling cases.

19. In the formulation of this analysis, the incompressible skin friction law of Karman-Schoenherr has been used as a basis for the zero heat transfer case. Unfortunately, little experimental data are available which describe the influence of heat transfer on incompressible skin friction coefficients. The analysis can, however, be applied to this case and comparisons made with the few data that are available. The experimental results of reference (l), while not reported in sufficient detail to make an exact computation using the present analysis, may be used to show that it does predict qualitatively correct results. In using these experimental data for this comparison it is assumed that the ratio  $c_f/c_{f1}$  can be used interchangeably with  $C_f/C_{f1}$  and that little Reynolds number dependence on this ratio exists. Figure 6 shows both the predicted and experimental variation of  $c_f/c_{f1}$  with wall temperature ratio for a constant value of  $Re_0$  which represented a mean for the data of reference (l). The results shown in this figure demonstrate that the present analysis describes correctly the variation of  $c_f/c_{f1}$  with increasing wall temperature ratio. Figure 7 shows the influence of heat transfer parameter on the values of  $c_f/c_{f1}$  for several values of Mach number and a single value of  $Re_0$ . It is apparent that cooling of the surface results in an increase in the skin friction coefficient, whereas heating has the opposite effect. That this result is consistent with the incompressible results shown in Figure 6 is evident from the results shown in Figure 8. This figure shows the variation of  $c_f/c_{f1}$  with Mach number for several constant values of  $T_w/T_{\infty}$ . The curves of constant  $T_w/T_{\infty}$  intercept the zero heat transfer curve at only one point. Each intercept occurs at the Mach number where  $T_w/T_{\infty} = T_e/T_{\infty}$ . A curve of the same appearance has been deduced by Seiff (reference m) from an empirical correlation of experimental data for Mach numbers up to about 5. A direct comparison between the results presented in Figure 8 and those reported in reference (m) is not valid because the curves of Figure 8 were computed for constant  $Re_0$  and depend somewhat on this Reynolds number, whereas those of reference (m) are assumed to be independent of Reynolds number based on distance from the leading edge.



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20. A comparison between specific values of experimental skin friction coefficients and the associated values predicted by the present analysis is shown in the following three figures. Figure 9 shows the variation of  $c_f/c_{f1}$  with Mach number for zero heat transfer. All of the experimental data (references a, b, c, f, k, n, o, and p) shown were normalized to a constant  $Re_\theta$  of 8000 and are either specifically for the case of zero heat transfer or were linearly extrapolated to the zero heat transfer condition. The scheme used for processing the heat transfer results is outlined in reference (c). Good agreement between theory and experiment is found for the entire range of Mach numbers for which experimental data are available. Figures 10 and 11 show comparisons between theoretical and experimental values of  $c_f/c_{f1}$  plotted as a function of heat transfer parameter for those experimental data taken under conditions of steady state heat transfer (references c, f, and k). For each of the sets of data shown, the variation of Reynolds number with heat transfer rate, if any, was considered in the theoretical calculations. It is significant to note that the results shown for the data of reference (c) indicate little variation of skin friction ratio with increasing heat transfer. From the present analysis it appears that the increase in Reynolds number, which accompanied the increase in heat transfer rate, so influenced the results as to obviate any increase in skin friction ratio. In general, the agreement between theory and experiment is satisfactory for each of the sets of data shown.

## CONCLUDING REMARKS

21. A theoretical investigation of compressible turbulent boundary layers with heat transfer has been conducted. This investigation is based on a simple flow model which is realistic for both the zero heat transfer and heat transfer conditions. The validity of the flow model assumed is demonstrated by comparisons between theoretical and experimental results. The theory is presented in such a fashion that values of skin friction may be calculated when either the Reynolds number based on boundary layer momentum thickness, total boundary layer thickness, or distance from the leading edge is given. Good agreement is demonstrated between theoretical and experimental values of skin friction coefficients, for both the zero and heat transfer conditions. It is shown that the predicted influence of heat transfer and Reynolds number on the properties at the edge of the laminar sublayer is consistent with the available experimental data for both incompressible and compressible flows. It is anticipated that, with the acquisition of additional data covering a broader range of conditions, improvements will be made in both the functional nature and accuracy of the analysis.

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APPENDIX A

General Relations for the Local  
Skin Friction Coefficient

1. The equation of motion to be satisfied by a boundary layer flowing on a flat plate in the absence of a pressure gradient is:

$$u \frac{du}{dx} + v \frac{du}{dy} = \frac{1}{\rho} \frac{d\tau}{dy} = \frac{1}{\rho} \frac{d}{dy} \left[ \mu \frac{du}{dy} + \rho \ell^2 \left( \frac{du}{dy} \right)^2 \right] \quad (A1)$$

The total shear stress at any point in the boundary layer is

$$\tau_{Lam.} + \tau_{Turb.} = \mu \frac{du}{dy} + \rho \ell^2 \left( \frac{du}{dy} \right)^2 \quad (A2)$$

Donaldson (reference e) assumed that the ratio of the total stress to the laminar stress at the edge of the laminar sublayer is a constant,

$$\frac{\tau_{Lam.} + \tau_{Turb.}}{\tau_{Lam.}} = r = \text{constant at } y = \delta_L \quad (A3)$$

Using this assumption, and evaluating Eq. A2 at  $y = \delta_L$  by using,

$$\frac{du}{dy} = \frac{u_\infty \delta_L}{n \delta} \frac{1-n}{\delta} \quad (A4)$$

which is obtained from the power profile (Eq. 1), it can be shown that the thickness ratio of the laminar sublayer is

$$\frac{\delta_L}{\delta} = \left[ \frac{n(r-1) \delta_L^2}{\ell^2 Re_\delta} \right]^{\frac{n}{n+1}} \quad (A5)$$

2. It may also be logically assumed that at  $y = \delta_L$ , the laminar shear stress is equal to the turbulent shear stress

$$\tau_{Lam.} = \tau_{Turb.} \quad \text{at } y = \delta_L$$

Evaluating  $\tau_{Turb.}$  using Eq. 1 and  $\tau_{Lam.}$  using Eq. 2 yields the following expression for the thickness ratio of the laminar

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sublayer

$$\frac{\delta_L}{\delta} = \left[ \frac{n^2 \delta^2}{\ell^2} \frac{1}{Re_s} \right]^{\frac{n}{1-n}} \quad (A6)$$

Equations (A5) and (A6) necessarily contain the so far undetermined mixing length " $\ell$ " for which either the Prandtl mixing length law

$$\ell = k y \quad (A7)$$

or the von Karman mixing length law

$$\ell = k \frac{du}{dy} \frac{dy^2}{d^2u} \quad (A8)$$

may be used.

3. It is evident therefore, that the assumptions used to obtain equations (A5) and (A6) together with the mixing length laws given in equations (A7) and (A8) will yield four equations for the thickness ratio of the laminar sublayer. These are tabulated below:

Assumption	Mixing length law	Laminar sublayer thickness ratio
Equation (A5)	Prandtl (Eq. A7)	$\frac{\delta_L}{\delta} = \left[ \frac{n(r-1)}{k^2 Re_s} \right]^{\frac{n}{n+1}}$
	von Karman (Eq. A8)	$\frac{\delta_L}{\delta} = \left[ \frac{n(r-1)}{k^2 Re_s} \right]^{\frac{n}{n+1}} \left[ \frac{1-n}{n} \right]^{\frac{2n}{n+1}}$
Equation (A6)	Prandtl (Eq. A7)	$\frac{\delta_L}{\delta} = \left[ \frac{n^2}{k^2 Re_s} \right]^{\frac{n}{n+1}}$
	von Karman (Eq. A8)	$\frac{\delta_L}{\delta} = \left[ \frac{n^2}{k^2 Re_s} \right]^{\frac{n}{n+1}} \left[ \frac{1-n}{n} \right]^{\frac{2n}{n+1}}$

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The local skin friction coefficient for incompressible flow may be calculated using the substitutions

$$\tau_w = \frac{u_L}{\delta_L}$$

$$\frac{u_L}{u_\infty} = \left( \frac{\delta_{L1}}{\delta} \right)^{\frac{1}{n}}$$

and

$$c_f = \frac{2 \tau_w}{\rho_\infty u_\infty^2}$$

together with each of the equations for the laminar sublayer thickness ratio. These are tabulated below.

Assumption	Mixing length law	Local skin friction coefficient law
Equation (A5)	Prandtl (Eq. A7)	$c_{f1} = 2 \left[ \frac{n(r-1)}{k^2} \right]^{\frac{1-n}{1+n}} \left[ \frac{1}{Re_\delta} \right]^{\frac{2}{n+1}} \quad (A9)$
	von Karman (Eq. A8)	$c_{f1} = 2 \left[ \frac{n(r-1)}{k^2} \right]^{\frac{1-n}{1+n}} \left[ \frac{1}{Re_\delta} \right]^{\frac{2}{n+1}} \left[ \frac{1-n}{n} \right]^{\frac{2(1-n)}{1+n}} \quad (A10)$
Equation (A6)	Prandtl (Eq. A7)	$c_{f1} = 2 \left[ \frac{n^2}{k^2} \right]^{\frac{1-n}{1+n}} \left[ \frac{1}{Re_\delta} \right]^{\frac{2}{n+1}} \quad (A11)$
	von Karman (Eq. A8)	$c_{f1} = 2 \left[ \frac{n^2}{k^2} \right]^{\frac{1-n}{1+n}} \left[ \frac{1}{Re_\delta} \right]^{\frac{2}{n+1}} \left[ \frac{1-n}{n} \right]^{\frac{2(1-n)}{1+n}} \quad (A12)$

APPENDIX B

Derivation of Local Skin Friction Coefficient  
Law for Compressible Turbulent  
Boundary Layers

1. It has been shown that equation (4) was the most suitable for incompressible turbulent boundary layers. This law is given as

$$c_{f_i} = 2 \left[ 20n \right]^{\frac{1-n}{1+n}} \left[ \frac{1}{Re_\delta} \right]^{\frac{2}{n+1}} \quad (4)$$

To extend this relation to compressible flows the property values (density and viscosity) need be evaluated at the edge of the laminar sublayer. Equation (4) may be written in the form

$$\frac{\tau_w}{\rho_\infty u_\infty^2} = \left[ 20n \right]^{\frac{1-n}{1+n}} \left[ \frac{\mu_\infty}{\rho_\infty u_\infty \delta} \right]^{\frac{2}{n+1}} \left[ \frac{\sqrt{\gamma_L}}{\sqrt{\gamma_\infty}} \right]^{\frac{2}{n+1}} \left[ \frac{\rho_L}{\rho_\infty} \right] \quad (B1)$$

using the following substitutions

$$\frac{\rho_L}{\rho_\infty} = \frac{T_\infty}{T_L}$$

and

$$\frac{\mu_L}{\mu_\infty} = \left[ \frac{T_L}{T_\infty} \right]^\omega$$

in equation (B1), yields the following relationship:

$$c_f = 2 \left[ 20n \right]^{\frac{1-n}{1+n}} \left[ \frac{1}{Re_\delta} \right]^{\frac{2}{n+1}} \left[ \frac{T_\infty}{T_L} \right]^{\frac{n-2\omega-1}{n+1}} \quad (B2)$$

2. To evaluate  $\frac{T_\infty}{T_L}$  it will be assumed that the Crocco quadratic form for the temperature distribution given as

$$T = A + B \left[ \frac{u}{u_\infty} \right] + C \left[ \frac{u}{u_\infty} \right]^2 \quad (B3)$$

is valid. By evaluating equation (B3) with the usual boundary conditions, the following equation results

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$$\frac{T_L}{T_\infty} = \frac{T_w}{T_\infty} - \left[ \frac{T_w - T_e}{T_\infty} \right] \left[ \frac{u_L}{u_\infty} \right] - \left[ \frac{T_e - T_\infty}{T_\infty} \right] \left[ \frac{u_L}{u_\infty} \right]^2 \quad (B4)$$

3. Equation (B4) may also be written as

$$\frac{T_L}{T_\infty} = 1 + \text{r.f.} \cdot \frac{\gamma-1}{2} M_\infty^2 \left[ 1 - \left( \frac{u_L}{u_\infty} \right)^2 \right] + \frac{T_w - T_e}{T_\infty} \left[ 1 - \frac{u_L}{u_\infty} \right] \quad (B5)$$

with the velocity ratio at the edge of the laminar sublayer given as

$$\frac{u_L}{u_\infty} = \left[ \frac{20n}{Re_\delta} \right]^{\frac{1}{n+1}} \left\{ 1 + \text{r.f.} \cdot \frac{\gamma-1}{2} M_\infty^2 \left[ 1 - \left( \frac{u_L}{u_\infty} \right)^2 \right] + \frac{T_w - T_e}{T_\infty} \left[ 1 - \frac{u_L}{u_\infty} \right] \right\}^{\frac{\omega+1}{n+1}} \quad (B6)$$

4. For all calculations using equations (B2), (B5) and (B6)  $\omega$  has been taken as 0.76 and the value of r.f. as 0.896.



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## APPENDIX C

### Derivation of Local and Average Skin Friction Coefficient Laws Based on $Re_x$

1. For incompressible flow the momentum equation for the boundary layer in the absence of a pressure gradient is

$$\frac{d\theta}{dx} = \frac{C_f}{2} \quad (C1)$$

or

$$\frac{dRe_\theta}{dRe_x} = \frac{C_f}{2} \quad (C2)$$

The following relation results when the right hand side of equation (4) is inserted into equation (C2);

$$\frac{dRe_\theta}{dRe_x} = \left[ 20n \right]^{\frac{1-n}{1+n}} \left[ \frac{1}{Re_\theta} \right]^{\frac{2}{n+1}} \left[ \frac{n}{(n+1)(n+2)} \right]^{\frac{2}{n+1}} \quad (C3)$$

and the substitution  $\frac{\delta}{\theta} = \frac{(n+1)(n+2)}{n}$  is used.

Equation (C3) can be integrated by assuming that  $n$  is a constant along a given plate (or  $\theta$  is constant). Whether or not this is a valid assumption will be verified by a comparison between the von Karman incompressible mean skin friction law and the derived relationship. Integrating equation (C3) yields

$$(Re_\theta)^{\frac{n+3}{n+1}} \cdot \frac{n+3}{n+1} \left[ \frac{1}{20n} \right]^{\frac{n-1}{n+1}} \left[ \frac{n}{(n+1)(n+2)} \right]^{\frac{2}{n+1}} Re_x \quad (C4)$$

and since

$$\frac{C_{fi}}{2} = \frac{Re_\theta}{Re_x} \quad (C5)$$

equation (C4) can be manipulated to yield

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$$\frac{C_{Fi}}{2} = \left\{ \left[ \frac{n+3}{n+1} \right] \left[ \frac{1}{20n} \right]^{\frac{n-1}{n+1}} \left[ \frac{n}{(n+1)(n+2)} \right]^{\frac{2}{n+1}} \right\}^{\frac{n+1}{n+3}} \left[ \frac{1}{Re_x} \right]^{\frac{2}{n+3}} \quad (C6)$$

A comparison between the values of  $C_{Fi}$  obtained from equation (C6) (using the  $n$  values associated with the  $Re_\theta$  values of figure 3 and equation (C4)) and the values of  $C_{Fi}$  from the von Karman mean skin friction equation for incompressible flow

$$\frac{0.242}{\sqrt{C_{Fi}}} = \log_{10} [C_{Fi} Re_x] \quad (C7)$$

indicated that over the Reynolds number ( $Re_x$ ) range from  $0.5 \times 10^6$  to  $60 \times 10^6$  the agreement between  $C_{Fi}$  values is within 4 percent. This result means that at least for incompressible flow the assumption that  $n$  is a constant along a plate can only lead to small errors in the estimation of skin friction values.

Using this information, the incompressible law for local skin friction coefficients on a  $Re_x$  basis may then be derived. The momentum equation can be written as

$$\frac{d\delta}{dx} = \frac{\delta}{2\theta} C_f \quad (C8)$$

Substituting equation (4) yields

$$\frac{d\delta}{dx} = \frac{\delta}{2\theta} \left[ 20n \right]^{\frac{1-n}{1+n}} \left[ \frac{1}{Re_\theta} \right]^{\frac{2}{n+1}} \left[ \frac{n}{(n+1)(n+2)} \right]^{\frac{2}{n+1}} \quad (C9)$$

which may be integrated to yield the following relation

$$\frac{Re_\delta}{Re_x} = \left[ \frac{n+3}{n+1} \left( \frac{\delta}{\theta} \right) \right]^{\frac{n+1}{n+3}} \left[ \frac{1}{20n} \right]^{\frac{n-1}{n+3}} \left[ \frac{1}{Re_x} \right]^{\frac{2}{n+3}} \quad (C10)$$

By inserting equation (C10) into equation (C3) the following local skin friction law results

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$$\frac{C_{fi}}{2} = \left[ \frac{1}{20n} \right]^{\frac{n-1}{n+3}} \left[ \frac{n+1}{n+3} \left( \frac{\theta}{5} \right) \right]^{\frac{2}{n+3}} \left[ \frac{1}{Re_x} \right]^{\frac{2}{n+3}} \quad (C11)$$

or

$$\frac{C_{fi}}{2} = \left[ \frac{1}{20n} \right]^{\frac{n-1}{n+3}} \left[ \frac{n}{(n+2)(n+3)} \right]^{\frac{2}{n+3}} \left[ \frac{1}{Re_x} \right]^{\frac{2}{n+3}} \quad (C12)$$

2. For compressible flow the extension of the foregoing expressions for the mean and local skin friction coefficients to compressible flows necessitates the use of an additional approximation the accuracy of which is checked with the available experimental data.

The local skin friction law (equation B2)

$$\frac{C_f}{2} = \left[ \frac{1}{20n} \right]^{\frac{n-1}{n+1}} \left[ \frac{1}{Re_\delta} \right]^{\frac{2}{n+1}} \left[ \frac{T_\infty}{T_L} \right]^{\frac{n-2.52}{n+1}} \quad (B2)$$

embodies the term  $\left( \frac{T_\infty}{T_L} \right)$  which cannot be a predetermined constant because it depends on Reynolds number as can be seen in the following equations:

$$\frac{T_L}{T_\infty} = 1 + r.f. \frac{\gamma-1}{2} M_\infty^2 \left[ 1 - \left( \frac{u_L}{u_\infty} \right)^2 \right] + \frac{T_w - T_e}{T_\infty} \left[ 1 - \frac{u_L}{u_\infty} \right] \quad (C13)$$

where

$$\frac{u_L}{u_\infty} = \left[ \frac{20n}{Re_\delta} \right]^{\frac{1}{n+1}} \left[ \frac{T_L}{T_\infty} \right]^{\frac{1.76}{n+1}} \quad \begin{matrix} (B6) \\ \text{or} \\ (C14) \end{matrix}$$

However, if  $\frac{T_\infty}{T_L}$  is assumed to be a constant that is associated with an average value of Reynolds number, the results that are obtained may be of sufficient accuracy for most applications. This is a logical step because for a given Mach number and heat transfer rate  $\frac{u_L}{u_\infty}$  is not seriously dependent

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on  $Re_s$  or  $Re_x$ . Using this assumption, the following relations may be derived from an integration of equation (B2).

$$\frac{C_F}{2} = \left\{ \left[ \frac{n+3}{n+1} \right]^{n+1} \left[ \frac{1}{20n} \right]^{n-1} \left[ \frac{\theta}{5} \right]^2 \left[ \frac{T_\infty}{T_L} \right]^{n-2.52} \left[ \frac{1}{Re_x} \right]^2 \right\}^{\frac{1}{n+3}} \quad (C15)$$

and

$$Re_s = \left[ \overline{Re_x} \right]^{\frac{n+1}{n+3}} \left[ \left( \frac{5}{\theta} \right) \right]^{n+1} \left( \frac{n+3}{n+1} \right)^{n+1} \left( \frac{1}{20n} \right)^{n-1} \left( \frac{T_\infty}{T_L} \right)^{n-2.52} \right]^{\frac{1}{n+3}} \quad (C16)$$

where  $\overline{Re_x}$  is given by

$$\overline{Re_x} = \frac{1}{2} Re_x \text{ (maximum)}$$

To determine local skin friction coefficients with the knowledge of only values of  $Re_x$  it is necessary to have available the variation of  $n$  with  $Re_x$  and  $Re_s$  for use in equation (C16). A calculation of the variation of  $n$  with  $Re_x$  and  $Re_s$  has been carried out for the zero heat transfer case and the results are plotted in figures 12 and 13 respectively. These calculations were made using the results tabulated in Table I, figure 3, and equations (C13) and (C14). Curves similar to those shown in figures 12 and 13 may be prepared for different heat transfer rates by the same method.

Using the data plotted in figures 12 and 13 the procedure for calculating  $C_f$  as a function of  $Re_x$  is as follows:

1. Determine the maximum value of  $Re_x$  to be encountered for a given problem. The selection of this value determines  $n$ ,  $Re_s$ , and  $Re_x$ .

2. Solve equation (C16) for  $\frac{T_\infty}{T_L}$ .

3. Insert the values of  $\frac{T_\infty}{T_L}$ ,  $n$ , and  $Re_s$  in equation (B2) and solve for  $C_f$ .

By a similar procedure equation (C15) may be used to calculate mean skin friction coefficients.

As a check on the approximate analysis described above, the variation of  $c_f/c_{f1}$  with Mach number has been carried out for three values of  $Re_x$  sufficient to encompass the  $Re_x$  range of the available experimental data. Figure 14 shows the

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results of these calculations compared to the available experimental data. The good agreement between theory and experiment tends to justify the approximations made in the preceding analysis.

Figure 15 shows the variation of the skin friction ratio with Mach number for a number of constant values of wall to free stream temperature ratio and a constant value of  $Re_x$  of  $10^7$ . The similarity between curves of this figure and the results plotted in figure 8 is apparent. However, differences in the curve shapes and corresponding values of the skin friction ratio can be seen by careful examination.

TABLE I

VARIATION OF DISPLACEMENT THICKNESS RATIO, $\frac{\delta^*}{\delta}$ , MOMENTUM THICKNESS RATIO, $\frac{\theta}{\delta}$ , AND BOUNDARY LAYER SHAPE PARAMETER WITH MACH NUMBER, $M$ , AND HEAT TRANSFER PARAMETER, $\frac{T_w - T_\infty}{T_\infty}$ , FOR A VELOCITY PROFILE EXPONENT, $n$ , OF 5.0						VARIATION OF DISPLACEMENT THICKNESS RATIO, $\frac{\delta^*}{\delta}$ , MOMENTUM THICKNESS RATIO, $\frac{\theta}{\delta}$ , AND BOUNDARY LAYER SHAPE PARAMETER WITH MACH NUMBER, $M$ , AND HEAT TRANSFER PARAMETER, $\frac{T_w - T_\infty}{T_\infty}$ , FOR A VELOCITY PROFILE EXPONENT, $n$ , OF 7.0					
$n$	$\frac{T_w - T_\infty}{T_\infty}$	$M$	$\frac{\delta^*}{\delta}$	$\frac{\theta}{\delta}$	$n$	$n$	$\frac{T_w - T_\infty}{T_\infty}$	$M$	$\frac{\delta^*}{\delta}$	$\frac{\theta}{\delta}$	$n$
3.0	0	0	0.10741	0.11893	1.40046	7.0	0	0	0.12449	0.09781	1.20874
		2.0	0.38470	0.08266	3.07232			2.0	0.32779	0.07861	2.80765
		4.0	0.46891	0.08843	7.99213			4.0	0.39944	0.08227	7.69287
		6.0	0.60324	0.02746	16.10281			6.0	0.52914	0.03479	18.49383
		8.0	0.89392	0.02843	37.36332			8.0	0.82887	0.05411	38.44484
		10.0	0.75960	0.01816	41.83921			10.0	0.71002	0.01786	40.43280
		12.0	0.80518	0.01354	59.46824			12.0	0.76187	0.01324	57.34532
		14.0	0.83844	0.01044	80.30651			14.0	0.80058	0.01028	77.80309
		16.0	0.86547	0.00829	104.28744			16.0	0.83018	0.00821	101.10040
		18.0	0.88732	0.00671	131.36482			18.0	0.85070	0.00670	127.32336
		20.0	0.89787	0.00558	161.78378			20.0	0.87120	0.00556	154.70673
5.0	2.0	0	0.33149	0.08204	4.04071	7.0	2.0	0	0.26818	0.07134	3.76474
		2.0	0.38674	0.08999	8.87030			2.0	0.32018	0.06181	8.34217
		4.0	0.38041	0.04977	19.84081			4.0	0.48278	0.04863	19.05352
		6.0	0.62891	0.02378	18.61783			6.0	0.86000	0.02168	17.88310
		8.0	0.70933	0.02374	39.87784			8.0	0.83344	0.02268	38.80889
		10.0	0.78737	0.01732	44.30716			10.0	0.71881	0.01678	42.81883
		12.0	0.80076	0.01306	61.91131			12.0	0.76712	0.01261	60.36360
		14.0	0.84127	0.01017	82.73232			14.0	0.80384	0.01004	80.07966
		16.0	0.86543	0.00811	106.70777			16.0	0.83471	0.00806	103.87843
		18.0	0.88410	0.00681	133.78189			18.0	0.85471	0.00689	129.89681
		20.0	0.89884	0.00547	164.31444			20.0	0.87438	0.00549	158.93332
5.0	4.0	0	0.48494	0.06438	6.89068	7.0	4.0	0	0.36822	0.05763	6.16081
		2.0	0.49007	0.08708	8.81899			2.0	0.49004	0.08164	7.74993
		4.0	0.86127	0.04897	13.06390			4.0	0.49484	0.03971	12.44983
		6.0	0.81068	0.03081	21.11632			6.0	0.86902	0.02909	20.84781
		8.0	0.72120	0.02819	32.35800			8.0	0.86187	0.02149	31.14943
		10.0	0.77437	0.01883	36.78184			10.0	0.77438	0.01810	48.11801
		12.0	0.81409	0.01264	64.40668			12.0	0.77308	0.01341	62.81968
		14.0	0.84417	0.00981	88.18668			14.0	0.80728	0.00979	82.46179
		16.0	0.86728	0.00784	109.23174			16.0	0.83485	0.00789	108.79814
		18.0	0.88548	0.00649	138.48327			18.0	0.85828	0.00648	132.14306
		20.0	0.89078	0.00540	166.83963			20.0	0.87339	0.00541	161.47674
5.0	6.0	0	0.48887	0.04338	9.18068	7.0	6.0	0	0.41899	0.04888	8.86897
		2.0	0.82127	0.04888	10.73944			2.0	0.48221	0.04464	10.12817
		4.0	0.82992	0.02818	28.86780			4.0	0.82002	0.02163	14.81068
		6.0	0.86920	0.02826	33.80014			6.0	0.86908	0.02894	33.60950
		8.0	0.73210	0.02101	34.84531			8.0	0.87880	0.02028	33.80617
		10.0	0.78087	0.01588	49.38414			10.0	0.73372	0.01345	47.48987
		12.0	0.81818	0.01224	66.84641			12.0	0.77679	0.01203	64.87190
		14.0	0.84685	0.00967	87.80014			14.0	0.81038	0.00917	84.88120
		16.0	0.86914	0.00779	111.84811			16.0	0.83879	0.00779	107.83308
		18.0	0.88670	0.00639	138.76389			18.0	0.85780	0.00639	124.84100
		20.0	0.90070	0.00533	168.96887			20.0	0.87488	0.00534	163.90120
5.0	8.0	0	0.83007	0.04006	11.42411	7.0	8.0	0	0.46688	0.04889	10.84738
		2.0	0.84168	0.04342	13.24140			2.0	0.48338	0.03947	12.80370
		4.0	0.82083	0.03438	18.03701			4.0	0.55653	0.03220	17.33910
		6.0	0.86561	0.02829	26.07826			6.0	0.82671	0.02811	24.88810
		8.0	0.74190	0.01989	37.80018			8.0	0.86787	0.01983	34.87700
		10.0	0.78692	0.01322	31.70171			10.0	0.74000	0.01486	49.83849
		12.0	0.83206	0.01186	69.31703			12.0	0.78128	0.01186	65.89112
		14.0	0.84943	0.00943	90.07423			14.0	0.81320	0.00924	87.08779
		16.0	0.87081	0.00763	114.14133			16.0	0.83888	0.00781	110.33653
		18.0	0.88784	0.00649	141.18057			18.0	0.86920	0.00689	138.81287
		20.0	0.90180	0.00528	171.40684			20.0	0.87877	0.00587	166.18890
5.0	10.0	0	0.87389	0.04088	14.18810	7.0	10.0	0	0.86880	0.03785	13.21440
		2.0	0.89399	0.03778	15.73092			2.0	0.89770	0.03466	14.87080
		4.0	0.84388	0.03123	20.83948			4.0	0.88010	0.02972	19.83330
		6.0	0.70001	0.02481	28.89877			6.0	0.84243	0.02382	27.20132
		8.0	0.75068	0.01889	39.77323			8.0	0.86928	0.01832	38.17688
		10.0	0.79288	0.01483	84.17638			10.0	0.74704	0.01432	88.16480
		12.0	0.81574	0.01180	71.80090			12.0	0.78138	0.01138	89.10700
		14.0	0.81890	0.00923	92.89783			14.0	0.81620	0.00912	99.49684
		16.0	0.87381	0.00749	118.80800			16.0	0.84090	0.00747	118.87028
		18.0	0.88918	0.00619	143.68109			18.0	0.86872	0.00620	138.82338
		20.0	0.90848	0.00519	173.89110			20.0	0.87683	0.00521	166.19178

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TABLE I (CONTINUED)

VARIATION OF DISPLACEMENT THICKNESS RATIO, $\frac{\delta^*}{\delta}$ , MOMENTUM THICKNESS RATIO, $\frac{\theta}{\delta}$ , AND BOUNDARY LAYER SHAPE PARAMETER WITH EACH NUMBER, $N$ , AND HEAT TRANSFER PARAMETER, $\frac{T_w - T_\infty}{T_\infty}$ , FOR A VELOCITY PROFILE EXPONENT, $n$ , OF 9.0						VARIATION OF DISPLACEMENT THICKNESS RATIO, $\frac{\delta^*}{\delta}$ , MOMENTUM THICKNESS RATIO, $\frac{\theta}{\delta}$ , AND BOUNDARY LAYER SHAPE PARAMETER WITH EACH NUMBER, $N$ , AND HEAT TRANSFER PARAMETER, $\frac{T_w - T_\infty}{T_\infty}$ , FOR A VELOCITY PROFILE EXPONENT, $n$ , OF 11.0					
$n$	$\frac{T_w - T_\infty}{T_\infty}$	$N$	$\frac{\delta^*}{\delta}$	$\frac{\theta}{\delta}$	$N$	$n$	$\frac{T_w - T_\infty}{T_\infty}$	$N$	$\frac{\delta^*}{\delta}$	$\frac{\theta}{\delta}$	$N$
9.0	0	0	0.10003	0.06100	1.22071	11.0	0	0	0.09371	0.07040	1.18009
		2.0	0.19941	0.08403	2.79877			2.0	0.18280	0.08994	2.73273
		4.0	0.38160	0.04714	7.45883			4.0	0.31436	0.04290	7.32323
		6.0	0.48992	0.02331	13.18040			6.0	0.45036	0.03013	14.08238
		8.0	0.59384	0.00800	21.01833			8.0	0.58937	0.01771	20.04296
		10.0	0.68911	0.01666	30.00000			10.0	0.63437	0.01618	29.03890
		12.0	0.78394	0.01983	38.47914			12.0	0.68416	0.01344	35.00396
		14.0	0.78830	0.01007	78.18983			14.0	0.74006	0.00981	78.44343
		16.0	0.80132	0.00806	98.17079			16.0	0.77884	0.00798	97.08433
		18.0	0.81784	0.00662	124.08466			18.0	0.80416	0.00680	123.73208
9.0	2.0	0	0.84790	0.00831	132.88388	11.0	2.0	0	0.83685	0.00542	132.36438
		2.0	0.88879	0.00883	3.00030			2.0	0.19388	0.05377	3.00198
		4.0	0.38390	0.08307	8.15320			4.0	0.24851	0.04961	8.02923
		6.0	0.40877	0.04117	9.78388			6.0	0.30280	0.03789	9.60148
		8.0	0.81716	0.02661	17.46707			8.0	0.47759	0.02777	17.19842
		10.0	0.60631	0.02188	28.10741			10.0	0.37105	0.02084	27.80428
		12.0	0.67921	0.01617	41.94187			12.0	0.64391	0.01334	41.43801
		14.0	0.73137	0.01348	58.73896			14.0	0.70038	0.01307	58.01988
		16.0	0.77807	0.00883	78.64837			16.0	0.74411	0.00959	77.58134
		18.0	0.80390	0.00793	101.80283			18.0	0.77864	0.00778	100.53805
9.0	4.0	0	0.83903	0.00836	127.18336	11.0	4.0	0	0.80614	0.00744	127.17081
		2.0	0.84951	0.00844	158.10794			2.0	0.82829	0.00540	153.38889
		4.0	0.39794	0.03184	5.03943			4.0	0.27171	0.04700	5.78063
		6.0	0.38034	0.04605	7.47706			6.0	0.31347	0.04278	7.30311
		8.0	0.44377	0.02871	13.08933			8.0	0.40302	0.03106	11.88449
		10.0	0.64077	0.00736	19.76606			10.0	0.50138	0.02580	19.42411
		12.0	0.68336	0.00508	20.47992			12.0	0.58535	0.01949	20.03382
		14.0	0.68670	0.01383	44.31784			14.0	0.65283	0.01486	43.03326
		16.0	0.73670	0.01207	61.03883			16.0	0.70604	0.01110	60.23861
		18.0	0.77588	0.00890	80.80206			18.0	0.74801	0.00836	79.91453
9.0	6.0	0	0.80638	0.00778	102.88059	11.0	6.0	0	0.78124	0.00782	102.83281
		2.0	0.83082	0.00641	129.06990			2.0	0.80806	0.00601	129.06658
		4.0	0.83049	0.00837	138.37889			4.0	0.82970	0.00328	136.83310
		6.0	0.39050	0.04402	8.28418			6.0	0.33943	0.04099	8.04396
		8.0	0.40137	0.04108	9.78847			8.0	0.38180	0.03784	9.58121
		10.0	0.47772	0.03321	14.38488			10.0	0.43759	0.03101	14.11188
		12.0	0.80148	0.02847	32.04384			12.0	0.52242	0.02410	31.67828
		14.0	0.83500	0.01939	39.74884			14.0	0.58946	0.01854	37.38129
		16.0	0.85483	0.01484	48.49284			16.0	0.66119	0.01441	45.88480
		18.0	0.74188	0.01173	83.94880			18.0	0.71188	0.01139	82.47388
9.0	8.0	0	0.77917	0.00937	83.18902	11.0	8.0	0	0.78178	0.00916	83.07484
		2.0	0.80679	0.00783	103.72349			2.0	0.78396	0.00749	104.07280
		4.0	0.83284	0.00631	131.93344			4.0	0.80994	0.00623	130.20900
		6.0	0.85173	0.00839	161.08079			6.0	0.83107	0.00523	158.91013
		8.0	0.41840	0.03937	18.88378			8.0	0.37540	0.03846	18.29622
		10.0	0.44829	0.03660	13.08743			10.0	0.40208	0.03403	11.81804
		12.0	0.80680	0.03037	18.67784			12.0	0.46833	0.02852	16.34993
		14.0	0.57989	0.02384	24.39466			14.0	0.54122	0.02286	23.90459
		16.0	0.64660	0.01844	36.05709			16.0	0.61052	0.01770	34.48323
		18.0	0.70207	0.01440	48.78994			18.0	0.68004	0.01362	48.08034
9.0	10.0	0	0.74878	0.01139	85.86629	11.0	10.0	0	0.71880	0.01110	84.37858
		2.0	0.76281	0.00917	85.33381			2.0	0.75534	0.00988	84.30804
		4.0	0.70907	0.00780	104.14667			4.0	0.78850	0.00738	104.88141
		6.0	0.81113	0.00780	124.11376			6.0	0.81138	0.00613	122.41087
		8.0	0.83432	0.00422	134.11376			8.0	0.83241	0.00517	141.00580
		10.0	0.85299	0.00522	163.40996			10.0	0.41330	0.03287	12.53464
		12.0	0.48389	0.03534	12.84380			12.0	0.42581	0.03162	14.04600
		14.0	0.47459	0.03215	14.25104			14.0	0.49137	0.02642	18.58251
		16.0	0.53172	0.02803	18.95440			16.0	0.55816	0.02135	26.14220
		18.0	0.59838	0.02242	36.60125			18.0	0.62165	0.01693	36.72180
9.0	10.0	0	0.65748	0.01763	37.28304	11.0	10.0	0	0.62165	0.01344	50.33462
		2.0	0.70907	0.01380	51.01459			2.0	0.72182	0.01020	44.88127
		4.0	0.78144	0.01148	87.82191			4.0	0.75884	0.00877	86.52723
		6.0	0.78573	0.00897	87.58197			6.0	0.78898	0.00724	104.46790
		8.0	0.81340	0.00734	110.51630			8.0	0.81356	0.00604	134.70199
		10.0	0.83585	0.00611	138.38213			10.0	0.83173	0.00517	162.83303
		12.0	0.85417	0.00517	165.22244			12.0	0.85417	0.00517	162.83303
		14.0	0.85417	0.00517	165.22244			14.0	0.85417	0.00517	162.83303
		16.0	0.85417	0.00517	165.22244			16.0	0.85417	0.00517	162.83303
		18.0	0.85417	0.00517	165.22244			18.0	0.85417	0.00517	162.83303
		20.0	0.85417	0.00517	165.22244			20.0	0.85417	0.00517	162.83303

TABLE I (CONTINUED)

VARIATION OF DISPLACEMENT THICKNESS RATIO, $\frac{\delta^*}{\delta}$ , MOMENTUM THICKNESS RATIO, $\frac{\theta}{\delta}$ , AND BOUNDARY LAYER SHAPE PARAMETER WITH MACH NUMBER, $M$ , AND HEAT TRANSFER PARAMETER, $\frac{T_w - T_e}{T_e}$ , FOR A VELOCITY PROFILE EXPONENT, $n$ , OF 5.0						VARIATION OF DISPLACEMENT THICKNESS RATIO, $\frac{\delta^*}{\delta}$ , MOMENTUM THICKNESS RATIO, $\frac{\theta}{\delta}$ , AND BOUNDARY LAYER SHAPE PARAMETER WITH MACH NUMBER, $M$ , AND HEAT TRANSFER PARAMETER, $\frac{T_w - T_e}{T_e}$ , FOR A VELOCITY PROFILE EXPONENT, $n$ , OF 7.0					
$n$	$\frac{T_w - T_e}{T_e}$	$M$	$\frac{\delta^*}{\delta}$	$\frac{\theta}{\delta}$	$H$	$n$	$\frac{T_w - T_e}{T_e}$	$M$	$\frac{\delta^*}{\delta}$	$\frac{\theta}{\delta}$	$H$
5.0	-2.0	4.0	0.39103	0.07235	5.39766	7.0	-2.0	4.0	0.33871	0.06304	5.21415
		6.0	0.57218	0.04215	13.37533			6.0	0.50724	0.03868	13.11272
		8.0	0.74046	0.02735	24.89540			8.0	0.62259	0.02586	24.05719
		10.0	0.75150	0.01909	39.37140			10.0	0.70087	0.01841	38.07170
		12.0	0.80032	0.01404	57.00142			12.0	0.75832	0.01372	55.12391
		14.0	0.84537	0.01074	77.78399			14.0	0.78702	0.01037	75.40206
		16.0	0.88144	0.00847	101.70012			16.0	0.82773	0.00839	98.45316
5.0	-4.0	18.0	0.91135	0.00684	128.83985	7.0	-4.0	18.0	0.85145	0.00681	125.03671
		20.0	0.93688	0.00563	159.30726			20.0	0.87011	0.00586	153.72798
		8.0	0.63339	0.04843	11.01383			8.0	0.48897	0.04473	10.70400
		10.0	0.68386	0.02986	22.27894			10.0	0.60422	0.02784	21.40259
		12.0	0.72943	0.02013	38.89021			12.0	0.69094	0.01932	35.76087
		14.0	0.76515	0.01437	54.87750			14.0	0.75442	0.01410	52.48231
		16.0	0.80234	0.01085	75.31222			16.0	0.78320	0.01085	73.11521
5.0	-6.0	18.0	0.85934	0.00885	99.34104	7.0	-6.0	18.0	0.82526	0.00839	96.07683
		20.0	0.87892	0.00695	126.60432			20.0	0.84974	0.00693	123.41143
		8.0	0.69387	0.00571	158.90018			8.0	0.41882	0.05066	8.26885
		10.0	0.48285	0.08738	8.41234			10.0	0.58326	0.03019	19.37097
		12.0	0.64360	0.02242	19.85811			12.0	0.69441	0.02038	33.40373
		14.0	0.73280	0.02131	34.38761			14.0	0.74418	0.01475	50.52274
		16.0	0.78962	0.01516	52.04443			16.0	0.78940	0.01118	70.73477
5.0	-8.0	18.0	0.85716	0.00884	96.98833	7.0	-8.0	18.0	0.82270	0.00705	94.02288
		20.0	0.87844	0.00708	124.08780			20.0	0.84789	0.00705	120.28269
		8.0	0.69493	0.00580	134.27586			8.0	0.40706	0.05079	149.86183
		10.0	0.62047	0.01583	17.31788			10.0	0.55900	0.03303	16.92401
		12.0	0.72196	0.02263	31.90455			12.0	0.68284	0.02153	31.03578
		14.0	0.78372	0.01580	49.60127			14.0	0.74418	0.01531	48.17113
		16.0	0.82525	0.01172	70.41909			16.0	0.78532	0.01148	68.40507
5.0	-10.0	18.0	0.85489	0.00905	94.46409	7.0	-10.0	18.0	0.80003	0.00894	91.73378
		20.0	0.87691	0.00721	121.82275			20.0	0.84618	0.00717	118.01953
		8.0	0.69377	0.00588	132.00680			8.0	0.40859	0.05087	147.58756
		10.0	0.59244	0.04619	14.73599			10.0	0.53041	0.03488	14.50766
		12.0	0.70991	0.02416	29.38328			12.0	0.65338	0.02285	28.87386
		14.0	0.77738	0.01650	47.15151			14.0	0.73040	0.01593	46.85080
		16.0	0.82152	0.01204	67.4872			16.0	0.78104	0.01189	66.07448
5.0		18.0	0.85353	0.00927	91.63332	7.0		18.0	0.81779	0.00915	89.32240
		20.0	0.87534	0.00735	119.08844			20.0	0.84433	0.00729	115.81619
		8.0	0.69688	0.00507	149.53099			8.0	0.40509	0.05096	145.15101
		10.0	0.59244	0.04619	14.73599			10.0	0.53041	0.03488	14.50766



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TABLE I (CONCLUDED)

VARIATION OF DISPLACEMENT THICKNESS RATIO, $\frac{\delta^*}{\delta}$ , MOMENTUM THICKNESS RATIO, $\frac{\theta}{\delta}$ , AND BOUNDARY LAYER SHAPE PARAMETER WITH MACH NUMBER, M, AND HEAT TRANSFER PARAMETER, $\frac{T_w - T_c}{T_\infty}$ , FOR A VELOCITY PROFILE EXPONENT, n, OF 9.0						VARIATION OF DISPLACEMENT THICKNESS RATIO, $\frac{\delta^*}{\delta}$ , MOMENTUM THICKNESS RATIO, $\frac{\theta}{\delta}$ , AND BOUNDARY LAYER SHAPE PARAMETER WITH MACH NUMBER, M, AND HEAT TRANSFER PARAMETER, $\frac{T_w - T_c}{T_\infty}$ , FOR A VELOCITY PROFILE EXPONENT, n, OF 11.0					
n	$\frac{T_w - T_c}{T_\infty}$	M <sub>∞</sub>	$\frac{\delta^*}{\delta}$	$\frac{\theta}{\delta}$	H	n	$\frac{T_w - T_c}{T_\infty}$	M <sub>∞</sub>	$\frac{\delta^*}{\delta}$	$\frac{\theta}{\delta}$	H
9.0	-2.0	4.0	0.29455	0.05567	5.11227	11.0	-2.0	4.0	0.23150	0.04946	5.04412
		6.0	0.43794	0.03561	12.85575			6.0	0.41870	0.02296	12.49172
		8.0	0.57628	0.02440	23.61885			8.0	0.53810	0.02306	23.35044
		10.0	0.63932	0.01782	37.41771			10.0	0.62414	0.01689	36.95086
		12.0	0.71950	0.01327	54.22005			12.0	0.68774	0.01284	53.55919
		14.0	0.76438	0.01031	74.14161			14.0	0.73583	0.01008	73.14115
		16.0	0.79868	0.00824	96.99981			16.0	0.77296	0.00866	95.80371
9.0	-4.0	18.0	0.82538	0.00672	122.82758	11.0	-4.0	18.0	0.80212	0.00660	121.85050
		20.0	0.84888	0.00558	151.72043			20.0	0.82537	0.00550	150.07273
		6.0	0.41884	0.02982	10.55481			6.0	0.38118	0.03638	10.42100
		8.0	0.53729	0.02614	21.31282			8.0	0.51874	0.02459	21.09394
		10.0	0.64874	0.01847	35.17182			10.0	0.61312	0.01765	34.75654
		12.0	0.71311	0.01372	51.97522			12.0	0.68097	0.01325	51.39623
		14.0	0.76028	0.01058	71.88200			14.0	0.73143	0.01031	70.94083
9.0	-6.0	16.0	0.79391	0.00740	94.75000	11.0	-6.0	16.0	0.78998	0.00823	93.94018
		18.0	0.82346	0.00684	120.39474			18.0	0.80003	0.00711	119.22504
		20.0	0.84519	0.00565	149.39292			20.0	0.82387	0.00557	147.91741
		6.0	0.37186	0.04542	8.19092			6.0	0.33548	0.04123	8.13738
		8.0	0.53582	0.02816	19.02899			8.0	0.49707	0.02839	18.83668
		10.0	0.63728	0.01940	33.85052			10.0	0.60121	0.01850	32.49730
		12.0	0.70833	0.01421	49.70443			12.0	0.67381	0.01370	49.18248
9.0	-8.0	14.0	0.75509	0.01047	69.54923	11.0	-8.0	14.0	0.72885	0.01057	64.77010
		16.0	0.79305	0.00859	92.32829			16.0	0.76892	0.00833	91.51551
		18.0	0.82149	0.00695	118.20144			18.0	0.79188	0.00705	116.96415
		20.0	0.84119	0.00572	147.51748			20.0	0.82253	0.00564	145.79787
		6.0	0.31123	0.03089	16.71134			6.0	0.47246	0.02850	16.57895
		8.0	0.52475	0.02044	20.98751			8.0	0.58828	0.01844	20.28235
		10.0	0.69813	0.01473	47.39661			10.0	0.68820	0.01421	46.80248
9.0	-10.0	12.0	0.78150	0.01117	67.27848	11.0	-10.0	12.0	0.72205	0.01085	64.85500
		14.0	0.79010	0.00877	90.09122			14.0	0.76371	0.00858	89.21739
		16.0	0.81947	0.00705	116.24113			16.0	0.79587	0.00892	114.81882
		18.0	0.84333	0.00588	145.24138			18.0	0.82075	0.00572	143.49650
		6.0	0.48883	0.03384	14.38879			6.0	0.44414	0.03104	14.30738
		8.0	0.81104	0.02181	28.37395			8.0	0.87417	0.02049	28.02143
		10.0	0.89165	0.01538	48.13704			10.0	0.85813	0.01473	44.87783
9.0	-10.0	12.0	0.74880	0.01149	84.98268	11.0	-10.0	12.0	0.71702	0.01118	84.50493
		14.0	0.78704	0.00898	87.85482			14.0	0.78040	0.00878	87.00878
		16.0	0.81738	0.00718	113.84401			16.0	0.79241	0.00704	112.69886
		18.0	0.84087	0.00580	142.52542			18.0	0.81914	0.00581	140.98107
		6.0	0.48883	0.03384	14.38879			6.0	0.44414	0.03104	14.30738
		8.0	0.81104	0.02181	28.37395			8.0	0.87417	0.02049	28.02143
		10.0	0.89165	0.01538	48.13704			10.0	0.85813	0.01473	44.87783

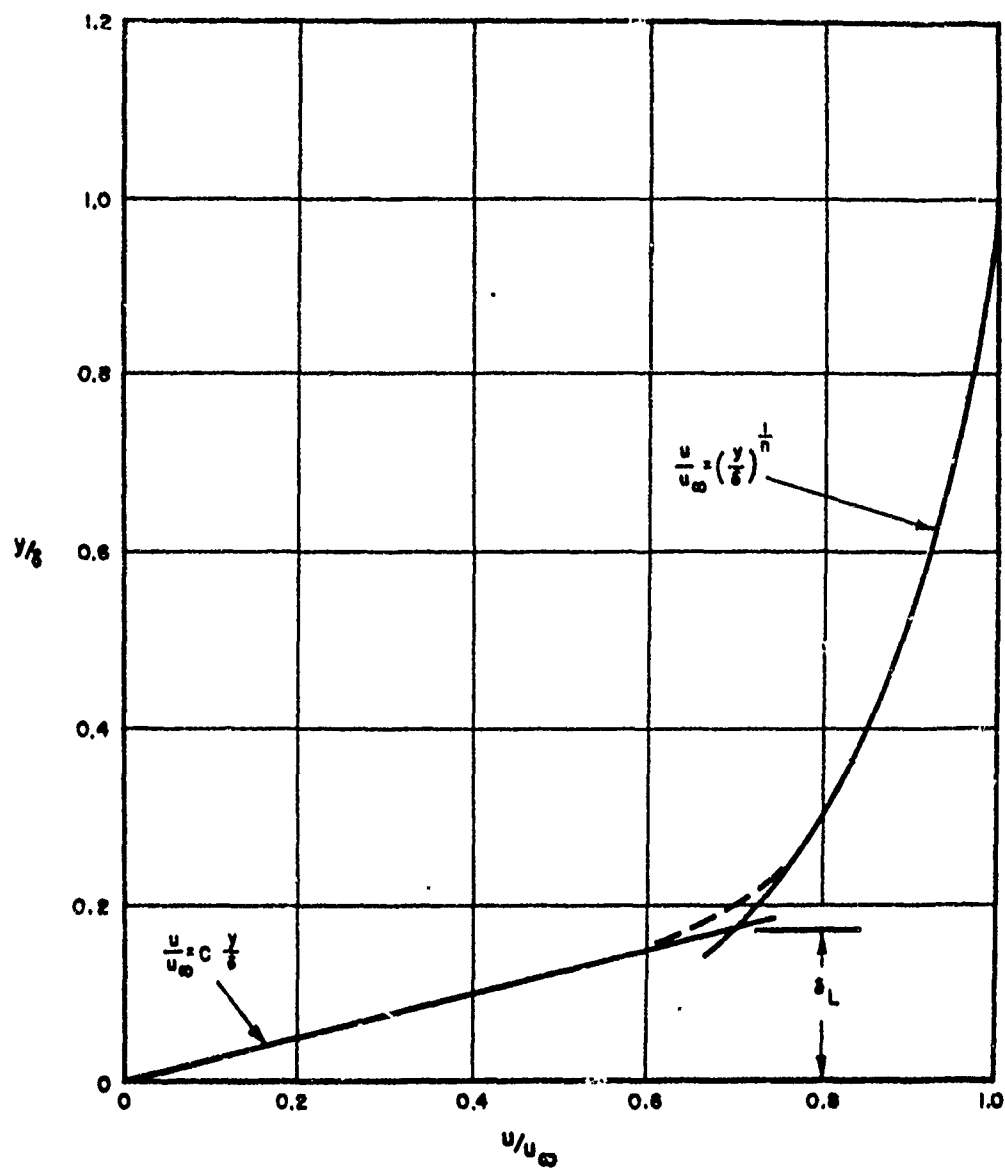


FIG.1 VELOCITY DISTRIBUTION ACROSS A TYPICAL TURBULENT BOUNDARY LAYER

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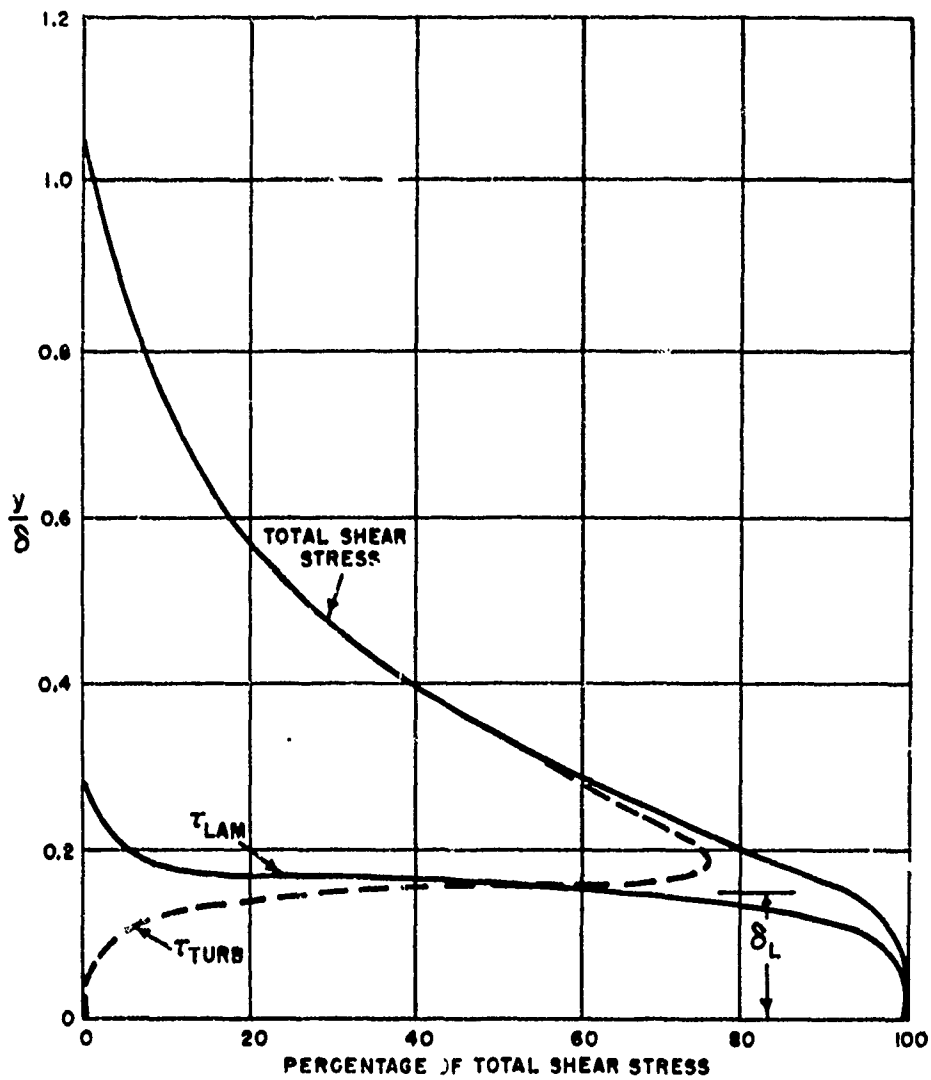
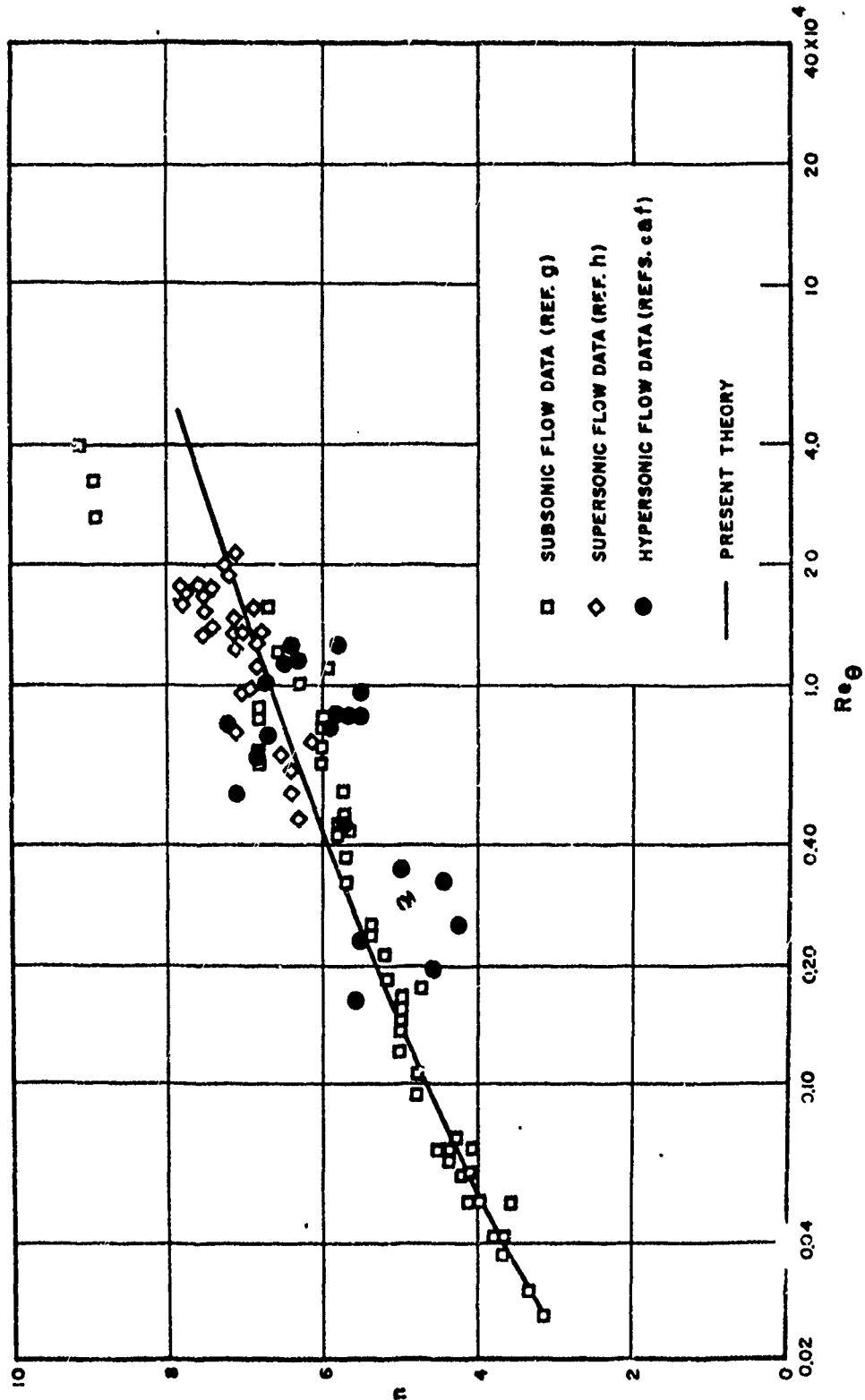


FIG. 2 SCHEMATIC VIEW OF VISCOUS AND TURBULENT SHEAR STRESS ACROSS A TYPICAL TURBULENT BOUNDARY LAYER



F 3.3 VARIATION OF TURBULENT BOUNDARY LAYER VELOCITY PROFILE EXPONENT ( $n$ )  
WITH REYNOLDS NUMBER ( $Re_\theta$ )

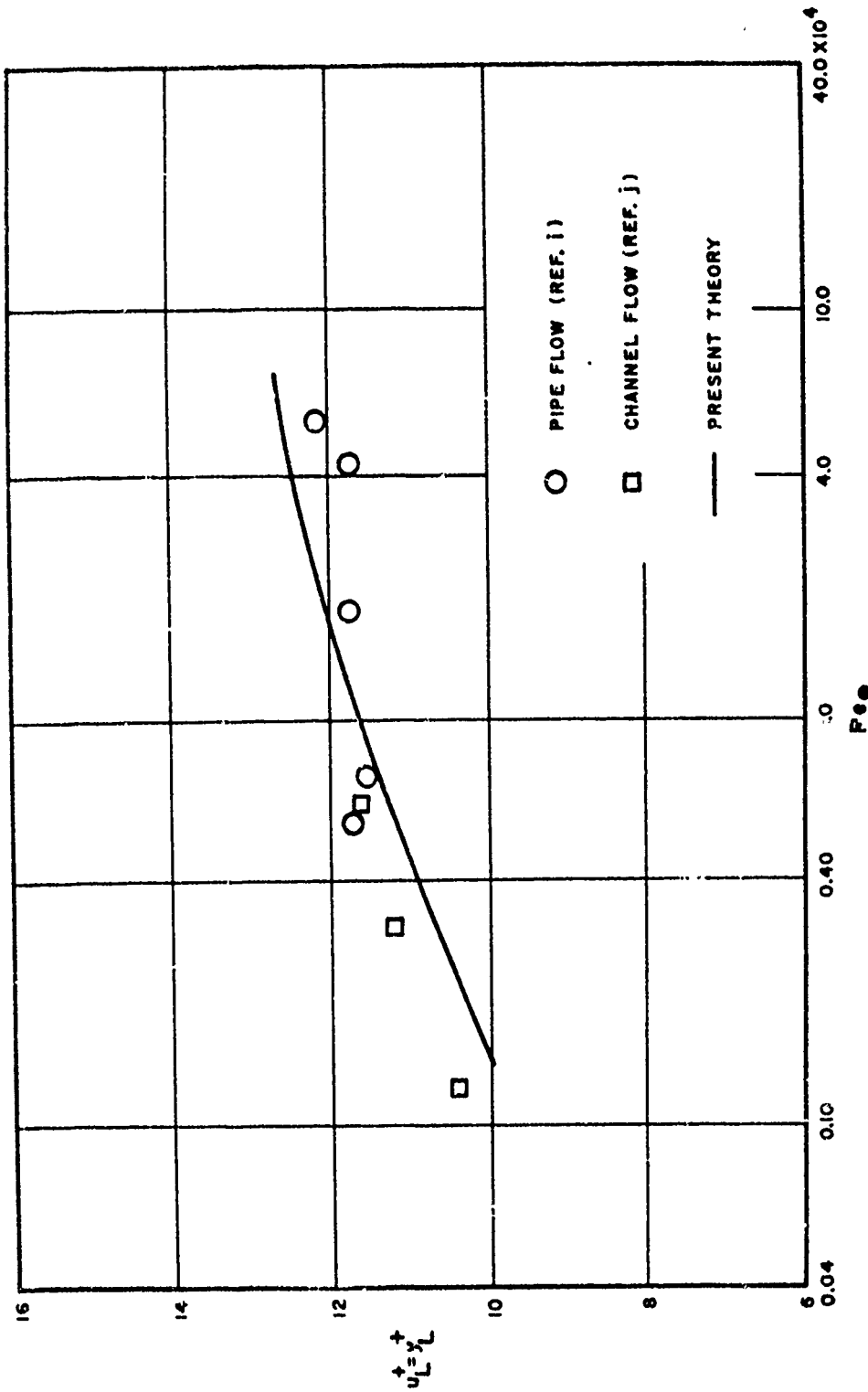


FIG. 4 VARIATION OF  $u_L^+ = y_L^+$  WITH REYNOLDS NUMBER ( $Re_0$ ) FOR INCOMPRESSIBLE FLOW

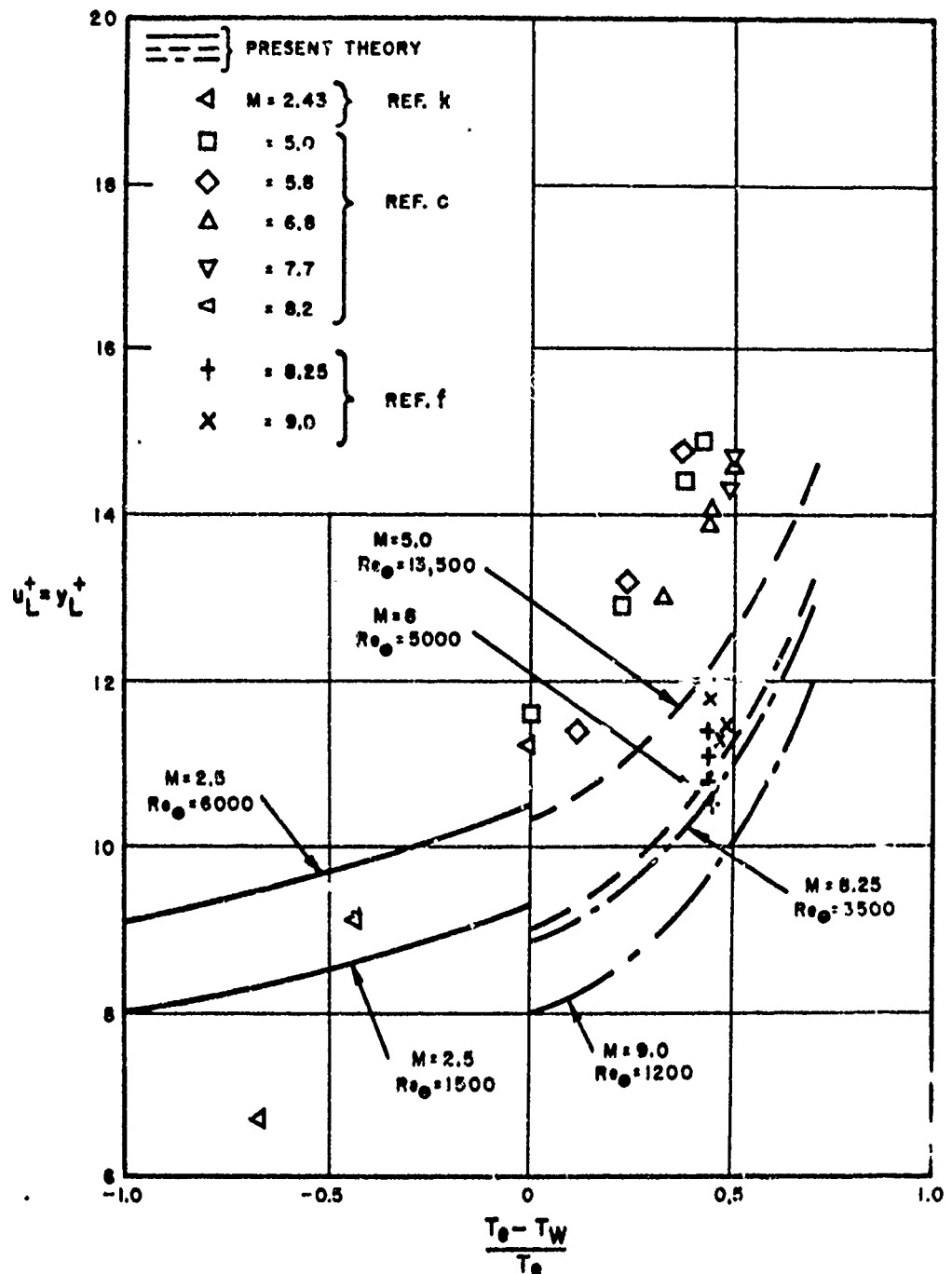


FIG. 5 COMPARISON BETWEEN THEORETICAL AND EXPERIMENTAL VALUES OF  $u_L^+ = y_L^+$  FOR COMPRESSIBLE FLOW

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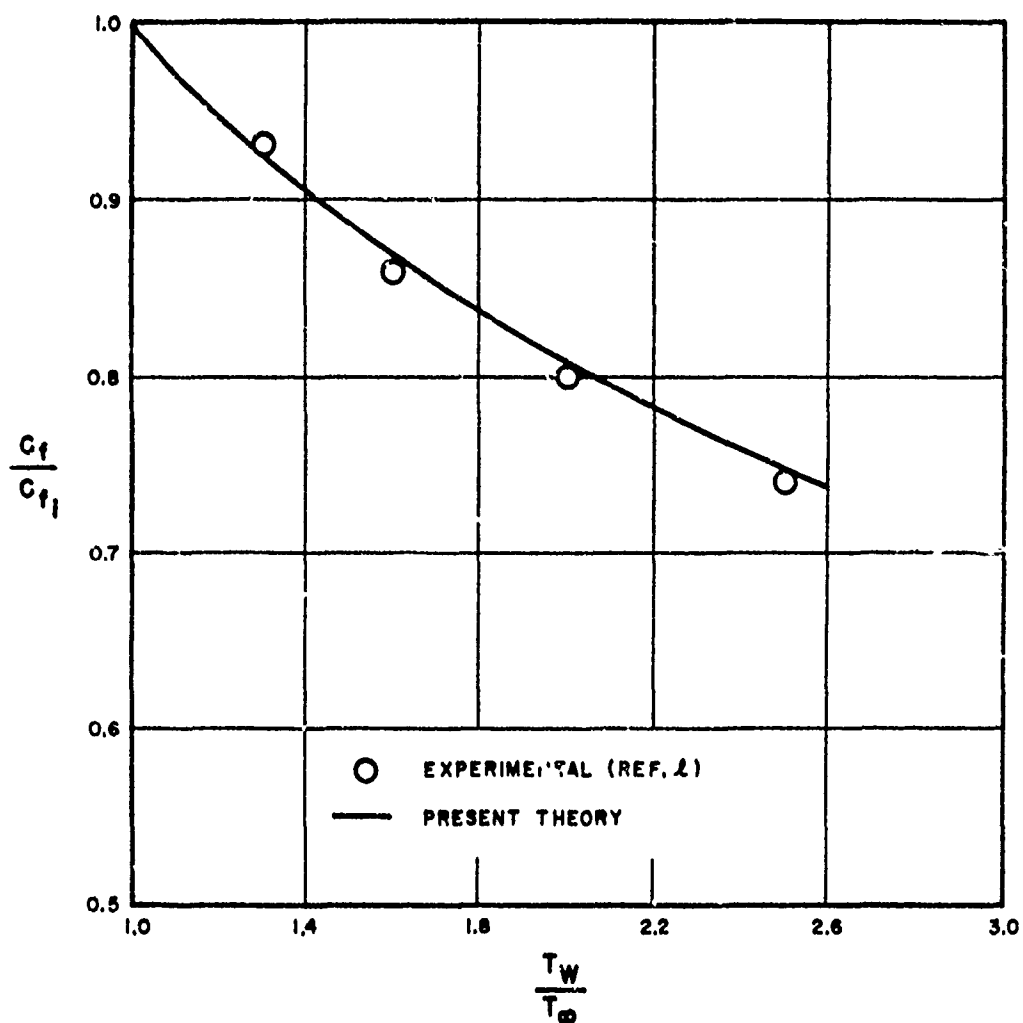


FIG. 6 INFLUENCE OF HEAT TRANSFER ON SKIN FRICTION RATIO FOR INCOMPRESSIBLE FLOW

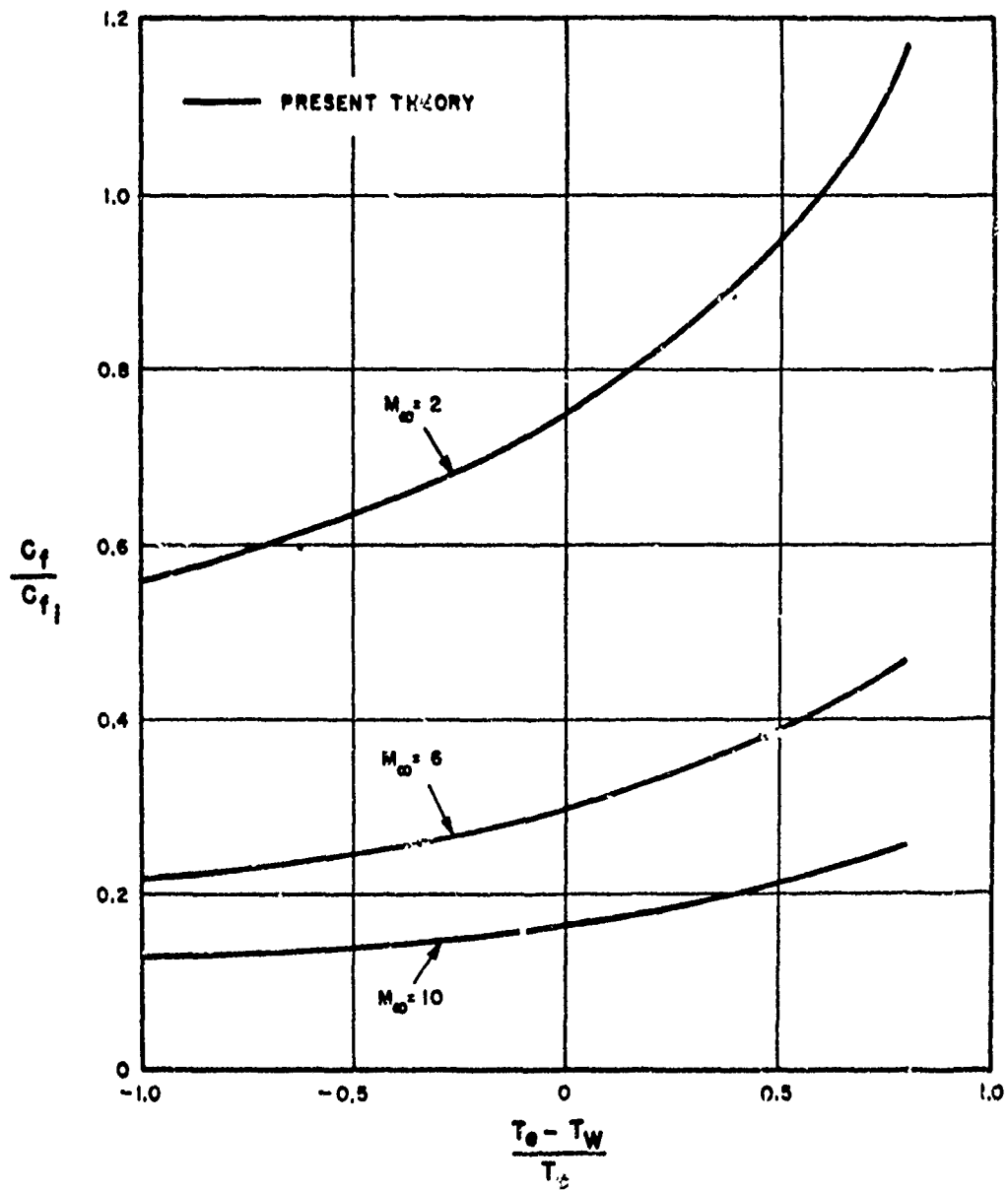


FIG. 7 INFLUENCE OF HEAT TRANSFER ON SKIN FRICTION RATIO FOR THREE VALUES OF MACH NUMBER AND  $Re_e = 13,500$



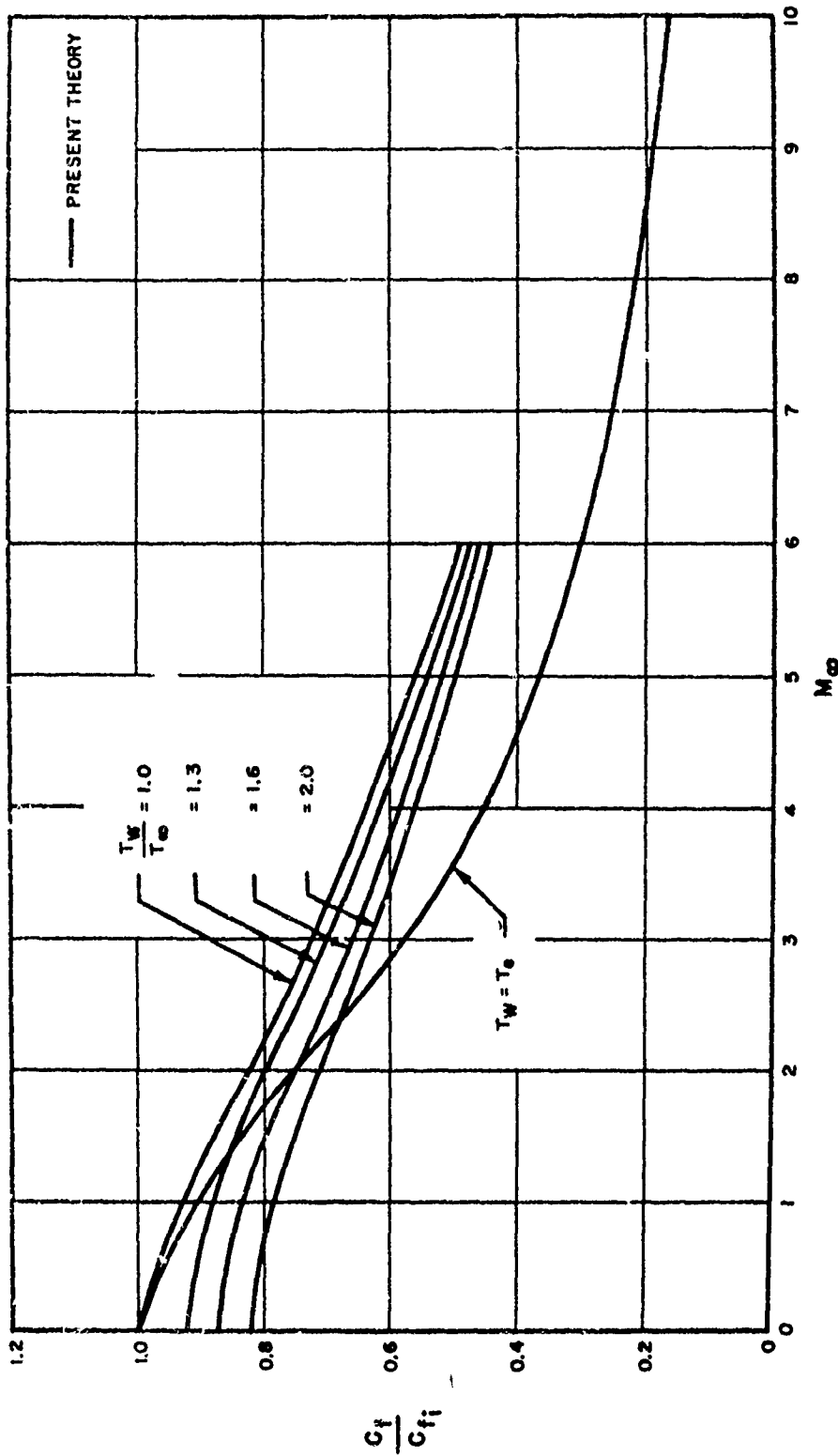


FIG. 8 VARIATION OF SKIN FRICTION RATIO WITH MACH NUMBER FOR SEVERAL CONSTANT VALUES OF WALL TO FREE STREAM TEMPERATURE RATIO AND  $Re_\theta = 13,500$

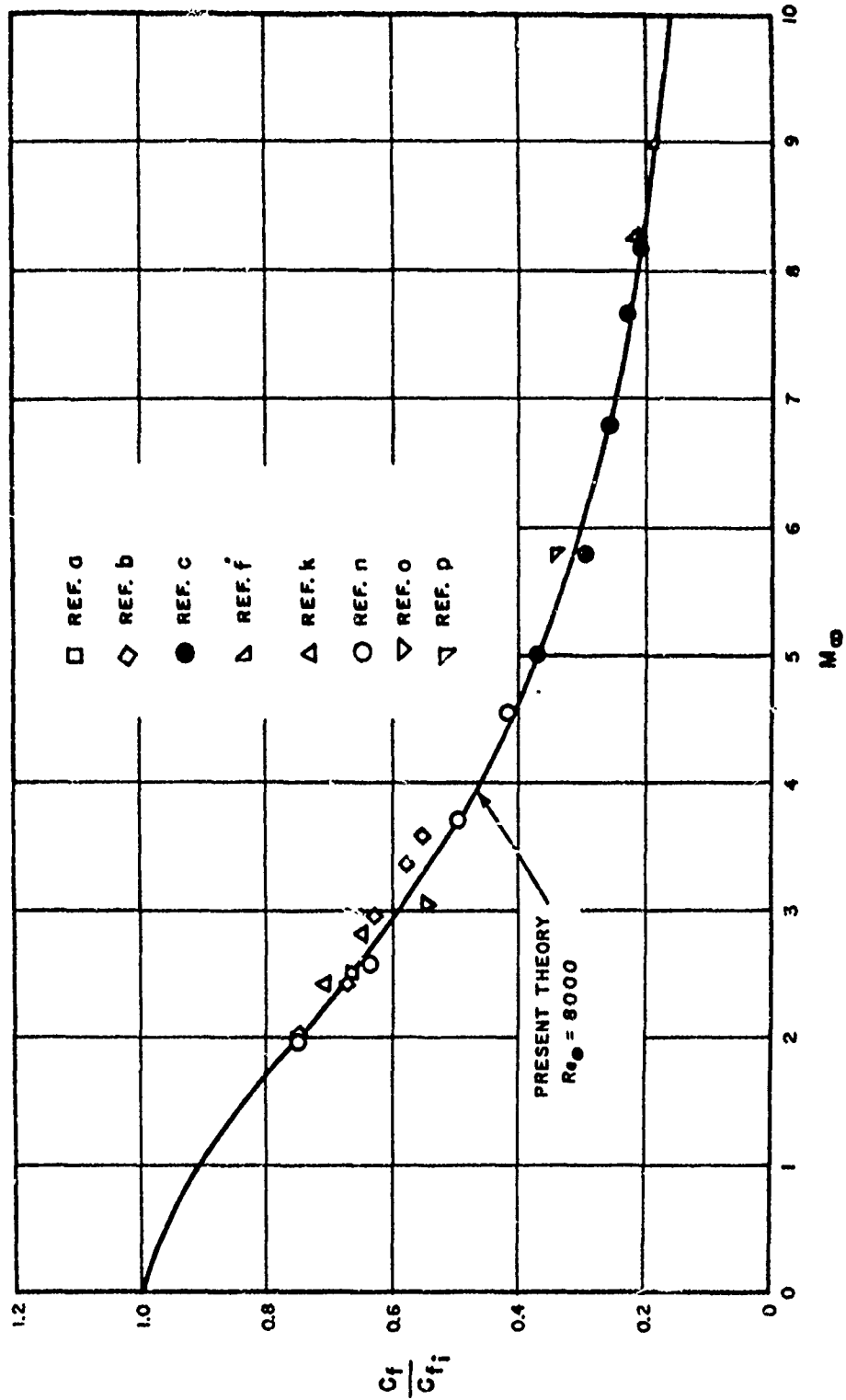


FIG. 9 VARIATION OF SKIN FRICTION RATIO WITH MACH NUMBER FOR ZERO HEAT TRANSFER AND  $Re_\theta = 8000$

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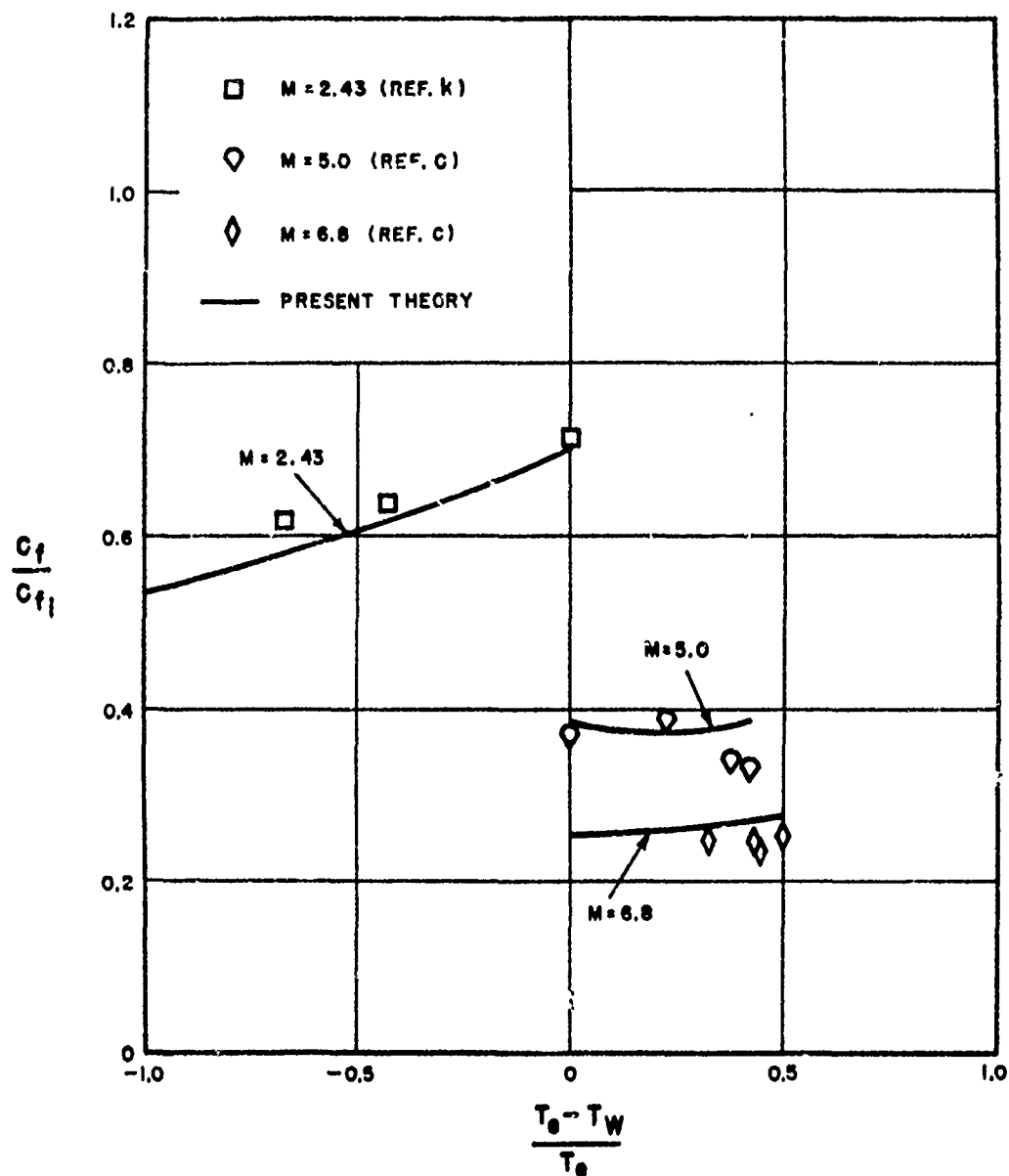


FIG. 10 COMPARISON BETWEEN THEORETICAL AND EXPERIMENTAL VALUES OF SKIN FRICTION RATIO FOR M=2.43, 5.0 AND 6.8

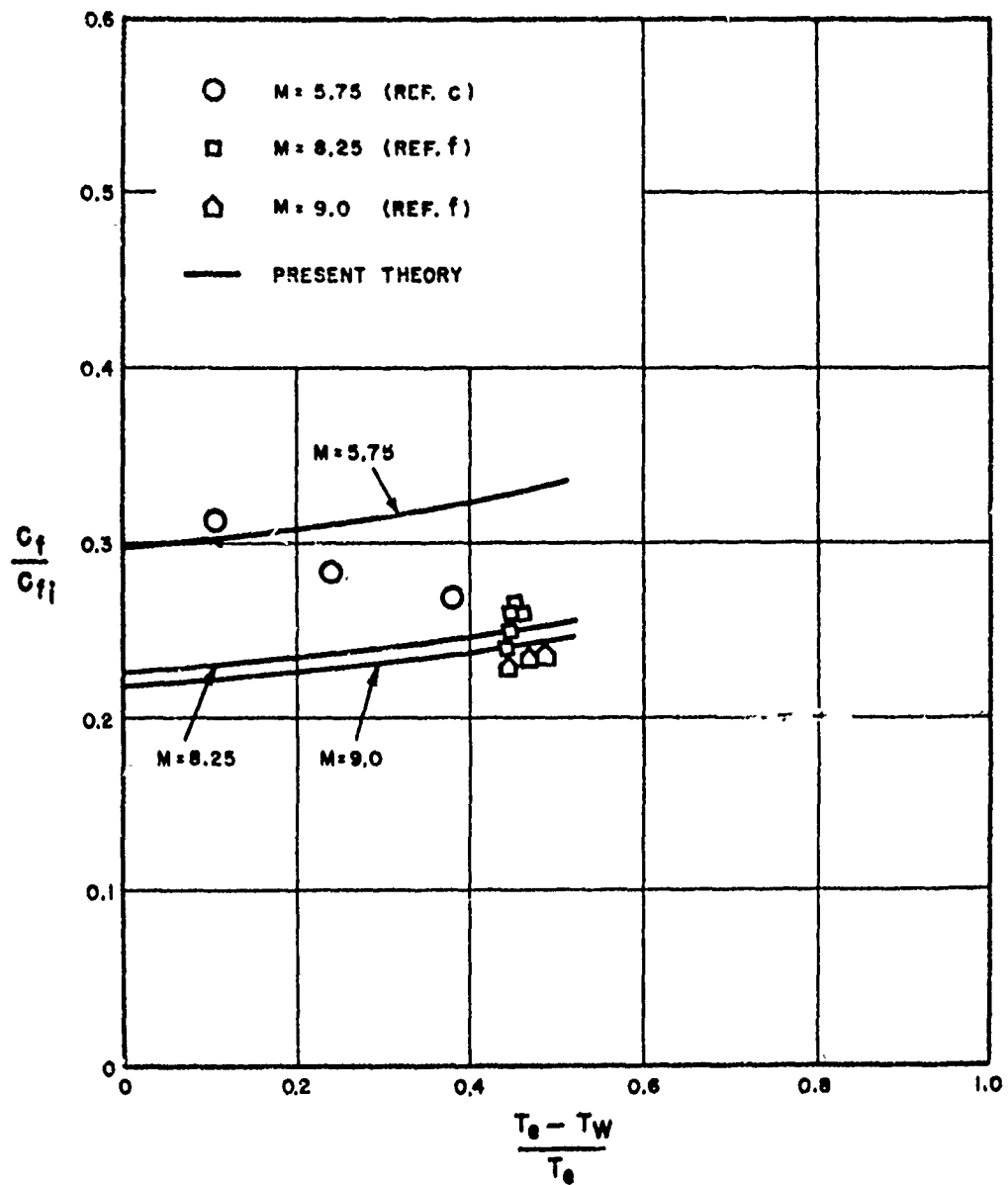


FIG. II COMPARISON BETWEEN THEORETICAL AND EXPERIMENTAL VALUES OF SKIN FRICTION RATIO FOR  $M=5.75, 8.25$ , AND  $9.0$

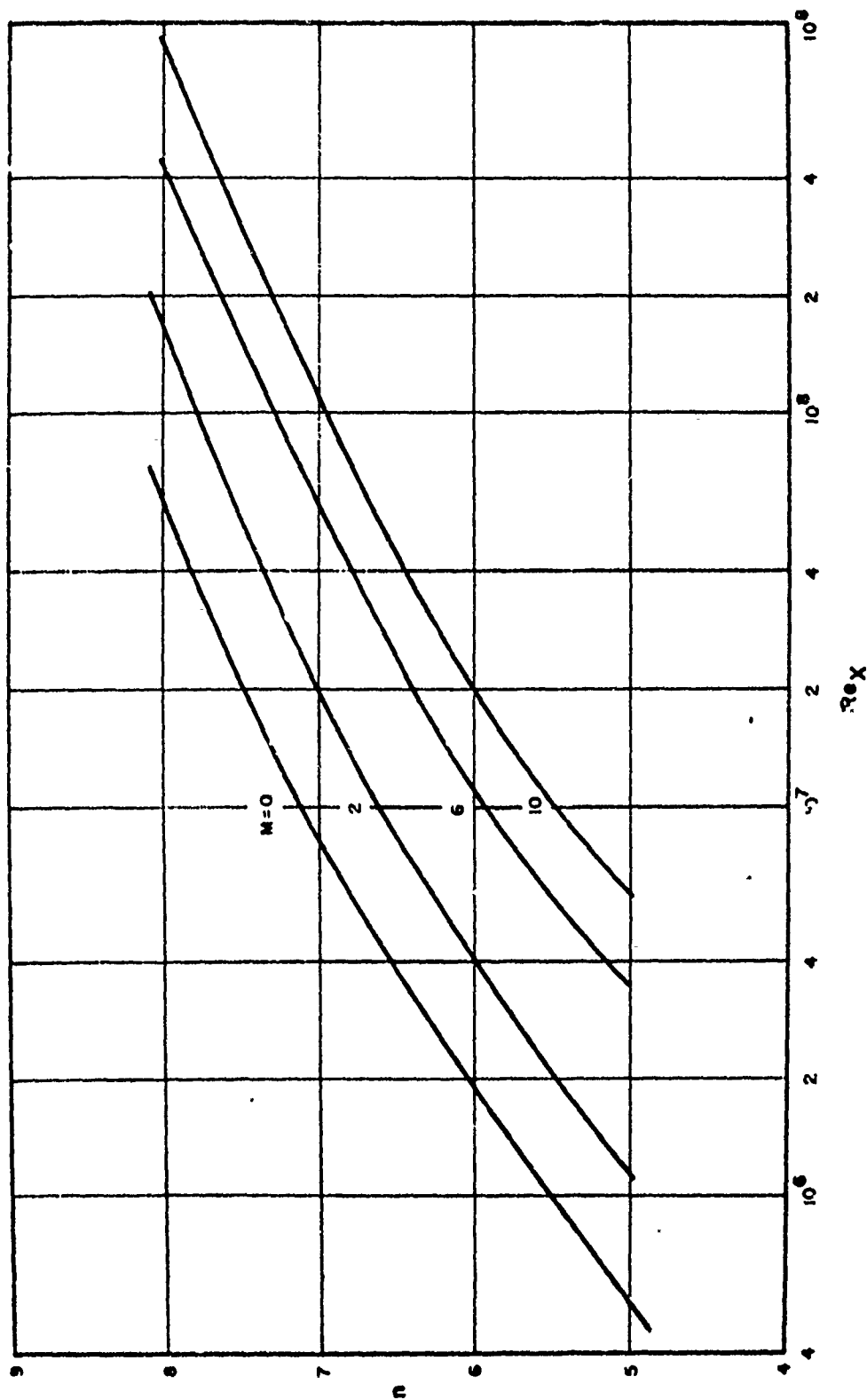


FIG.12 VARIATION OF  $n$  WITH  $Re_x$  FOR SEVERAL CONSTANT VALUES OF MACH NUMBER

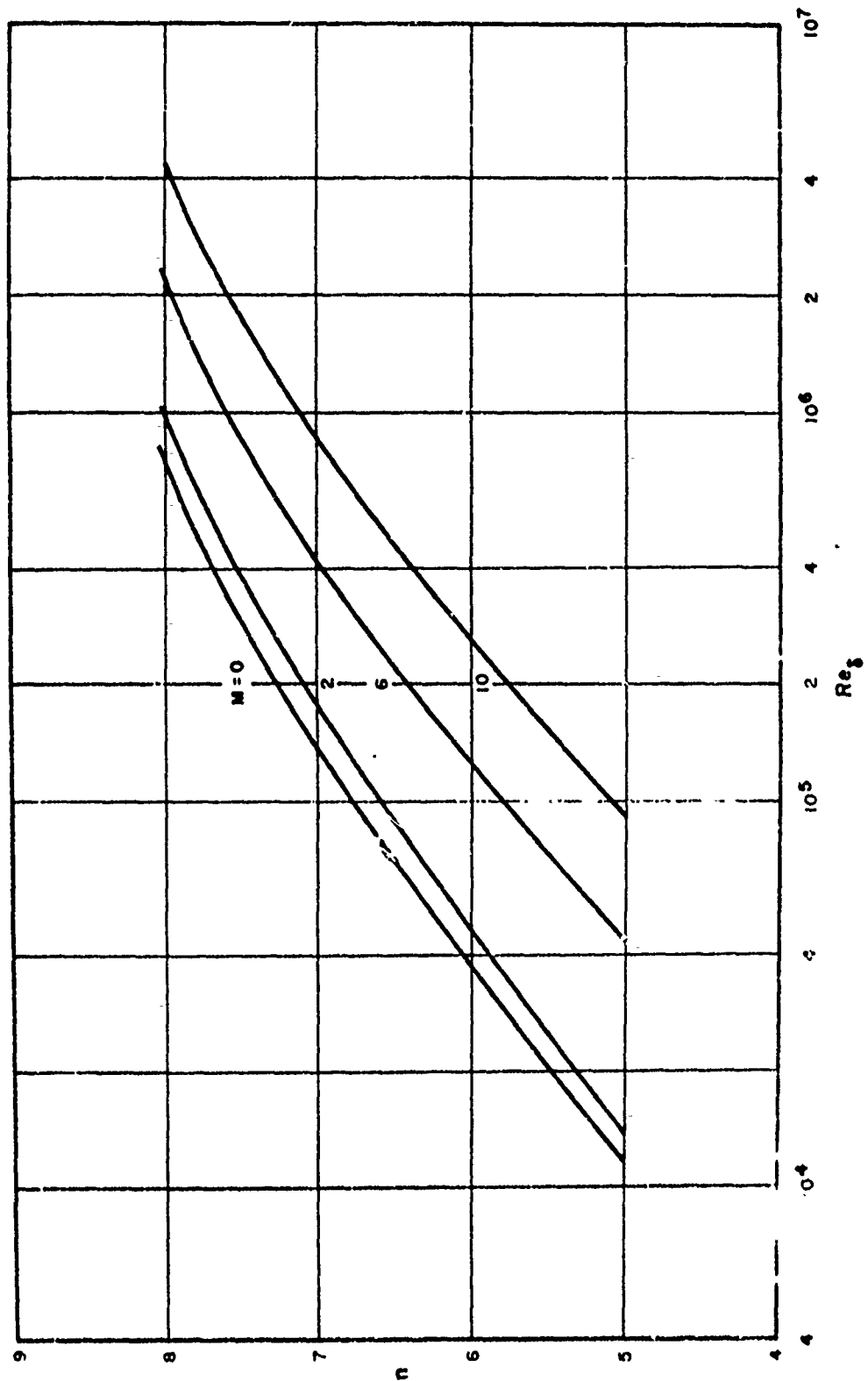


FIG. 13 VARIATION OF  $n$  WITH  $Re_\delta$  FOR SEVERAL CONSTANT VALUES OF MACH NUMBER

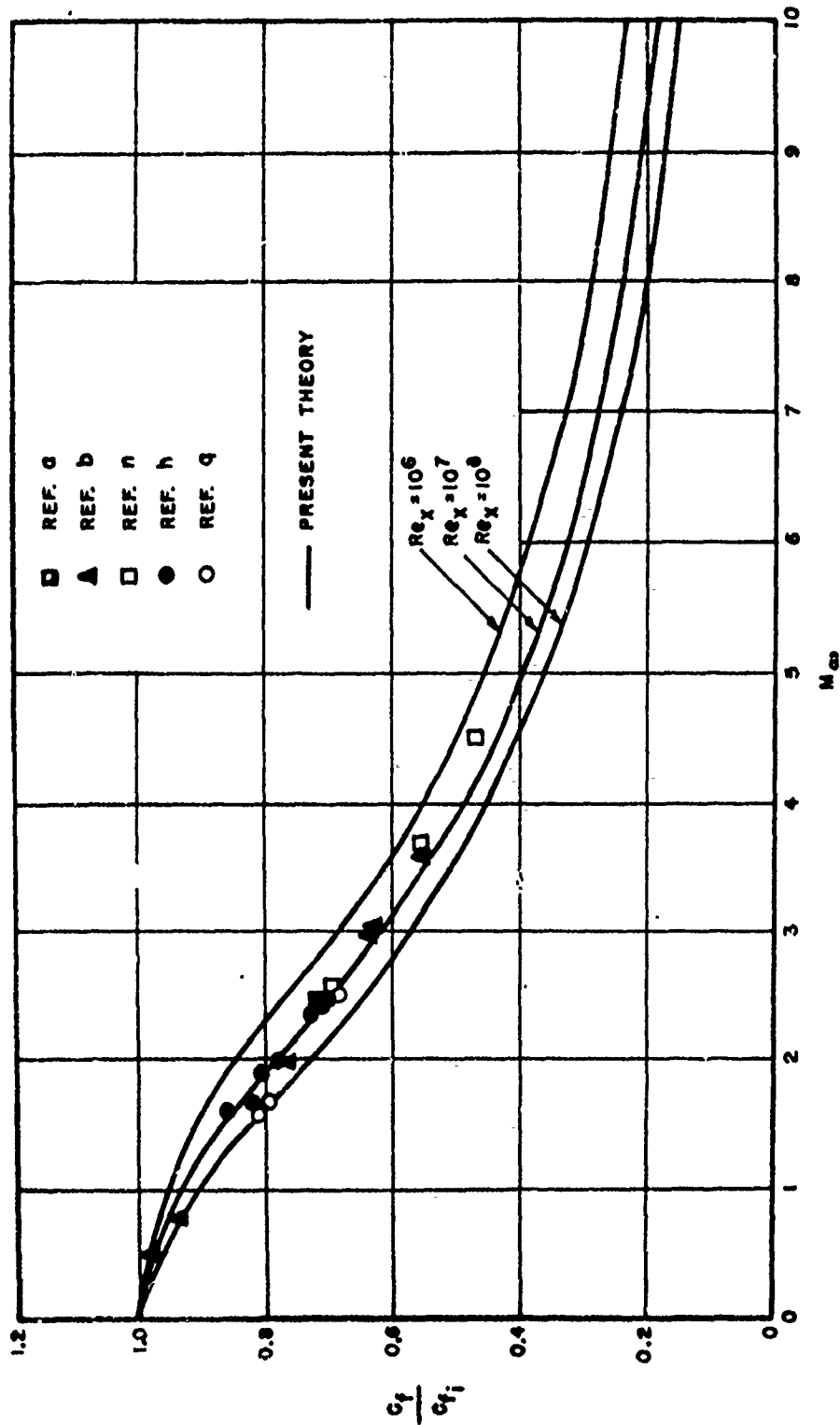


FIG. 14 VARIATION OF SKIN FRICTION RATIO WITH MACH NUMBER  
FOR CONSTANT VALUES OF  $Re_x$  OF  $10^6$ ,  $10^7$ , AND  $10^8$

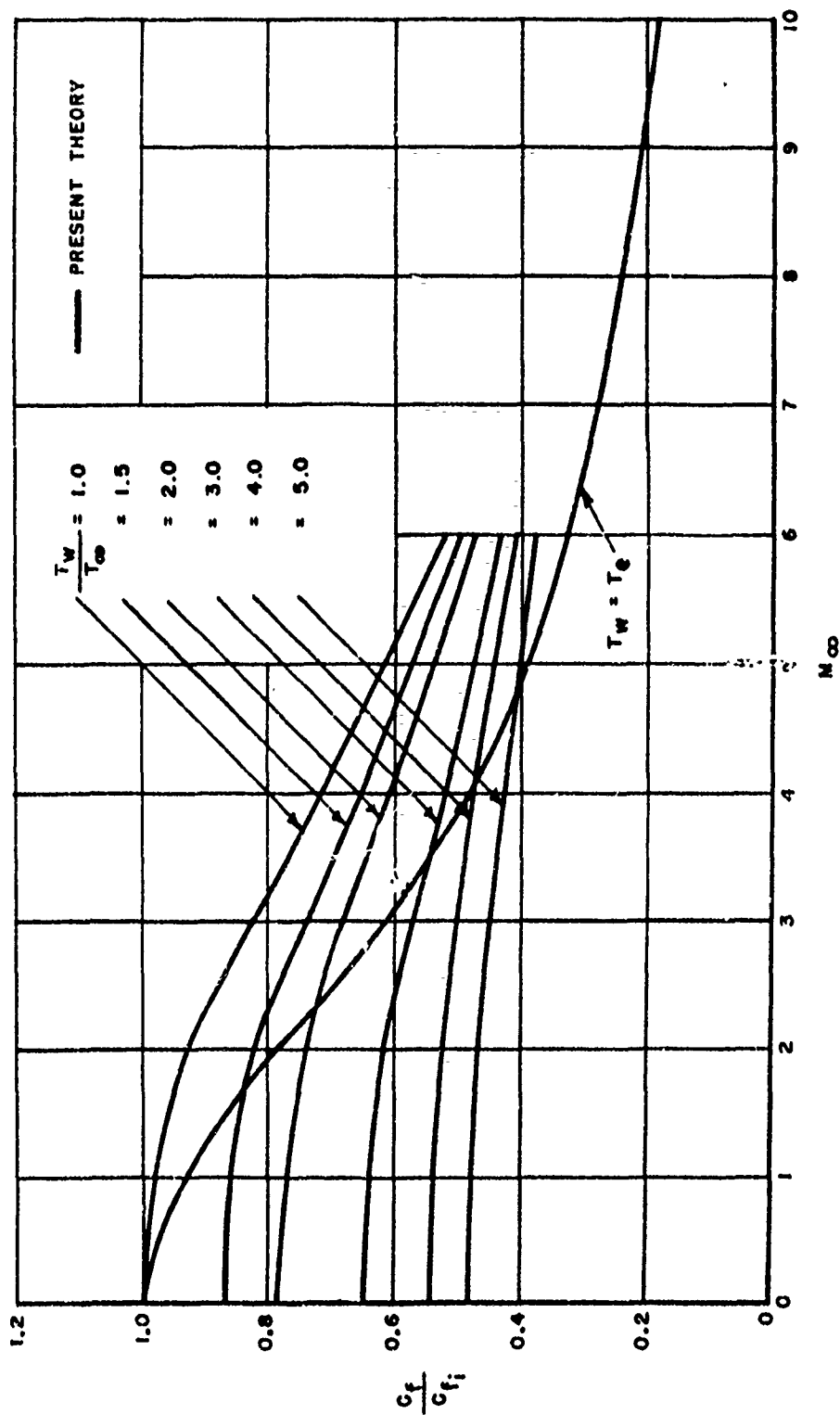


FIG. 15 VARIATION OF SKIN FRICTION RATIO WITH MACH NUMBER FOR SEVERAL CONSTANT VALUES OF WALL TO FREE-STREAM TEMPERATURE RATIO AND A CONSTANT  $Re_x$  OF  $10^7$



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